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Piotrowski et al.

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(54) **RECOMBINANT YEAST HAVING ENHANCED GAMMA VALEROLACTONE TOLERANCE AND METHODS OF USE**

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C12N 1/14 (2006.01)
C12N 15/81 (2006.01)

(52) **U.S. Cl.**
CPC **C12P 7/10** (2013.01); **C12N 1/14** (2013.01); **C12N 15/81** (2013.01); **Y02E 50/16** (2013.01)

(58) **Field of Classification Search**
None
See application file for complete search history.

(56) **References Cited**

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Mukai et al., "PAD1 and FDC1 are essential for the decarboxylation of phenylacrylic acids in *Saccharomyces cerevisiae*", Journal of Bioscience and Bioengineering, vol. 109, No. 6, pp. 564-569, 2010.*

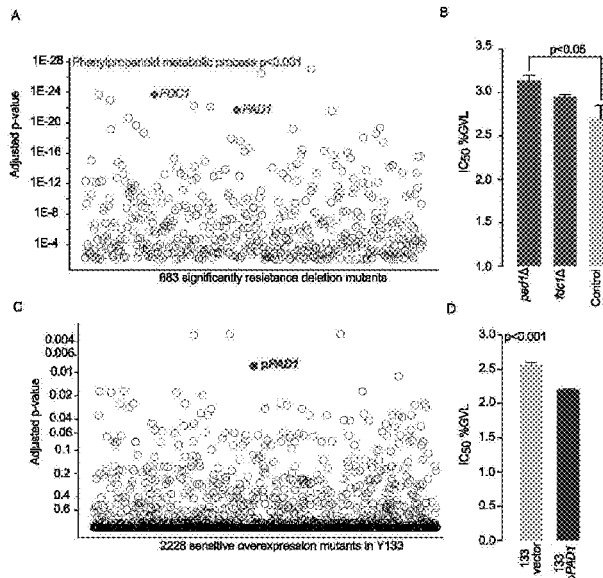
* cited by examiner

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(57) **ABSTRACT**

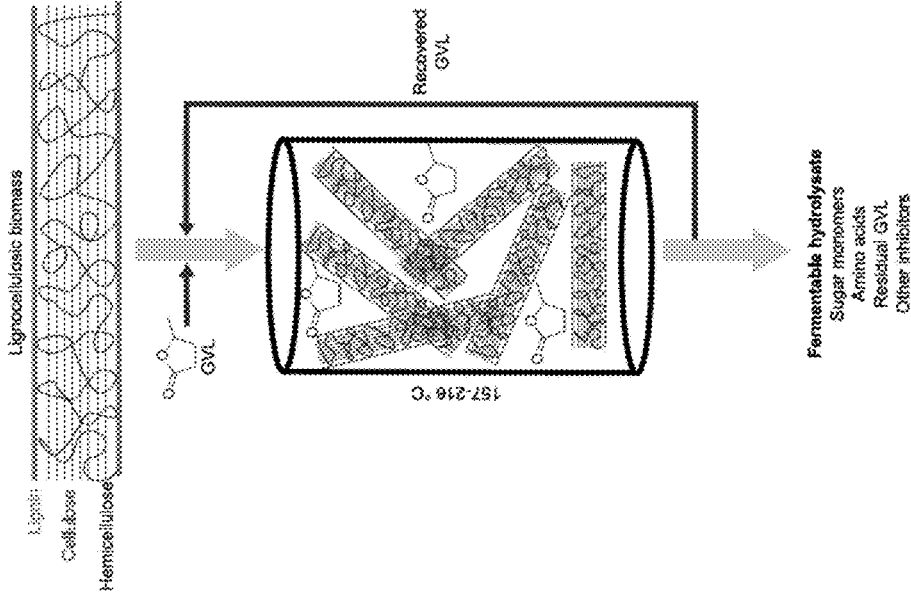
The present invention relates to materials and methods for the production of ethanol. More particularly, the present invention provides genetically modified strains of *Saccharomyces cerevisiae* having enhanced tolerance for gamma valerolactone (GVL) toxicity. Also provided are methods of using such genetically engineered yeast strains for improved GVL-mediated hydrolysis of lignocellulosic biomass for industrial-scale ethanol production.

22 Claims, 10 Drawing Sheets

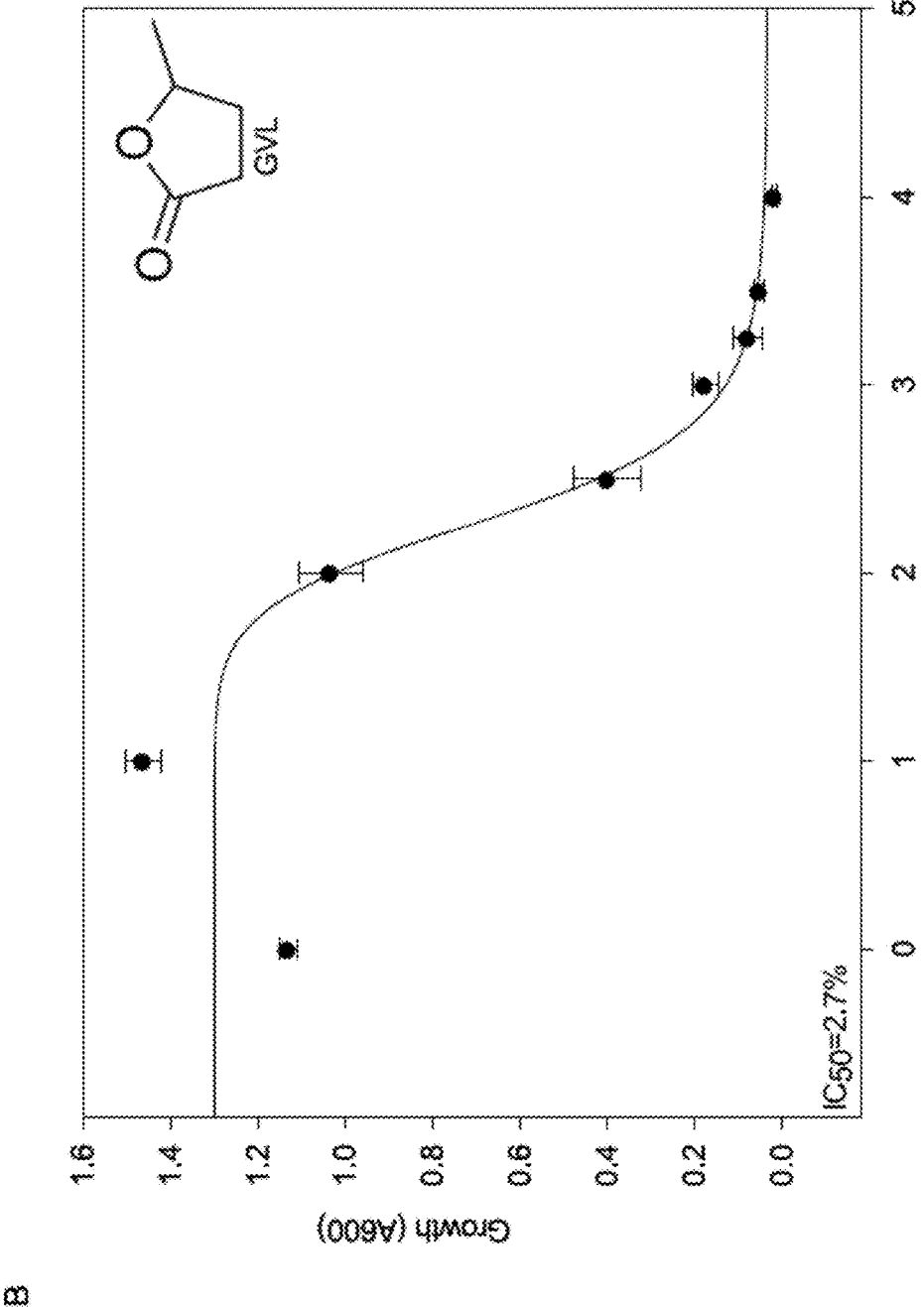


FIGS. 1A-1B

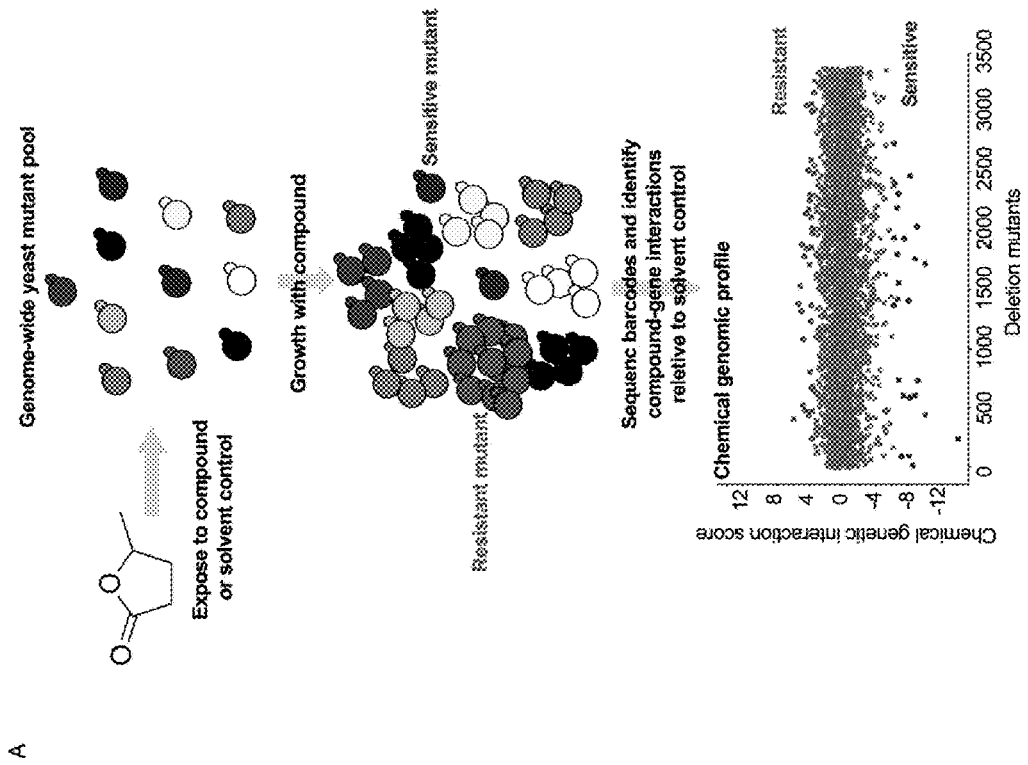
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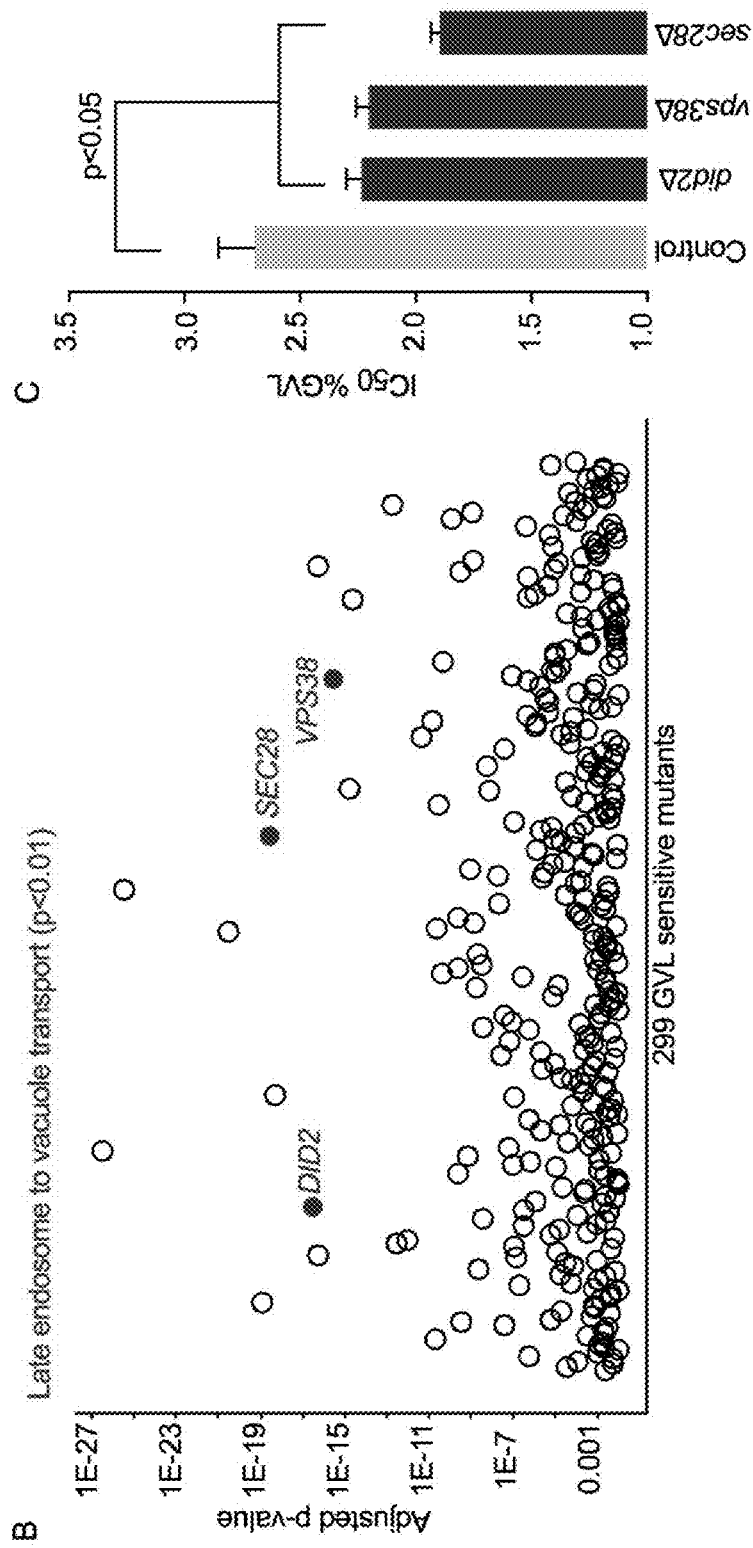
FIGS. 1A-1B, CONTINUED



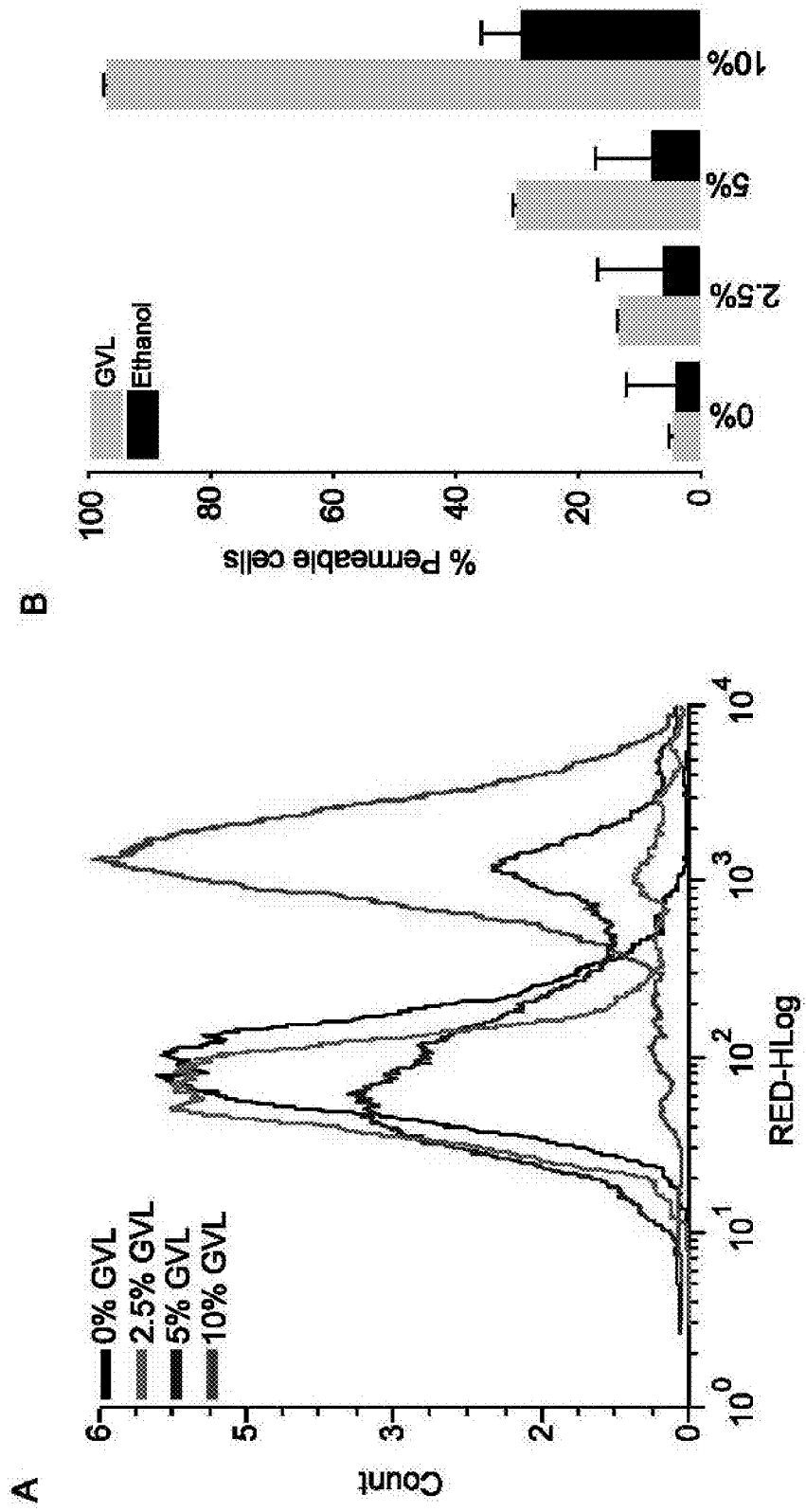
FIGS. 2A-2C



FIGS. 2A-2C, CONTINUED

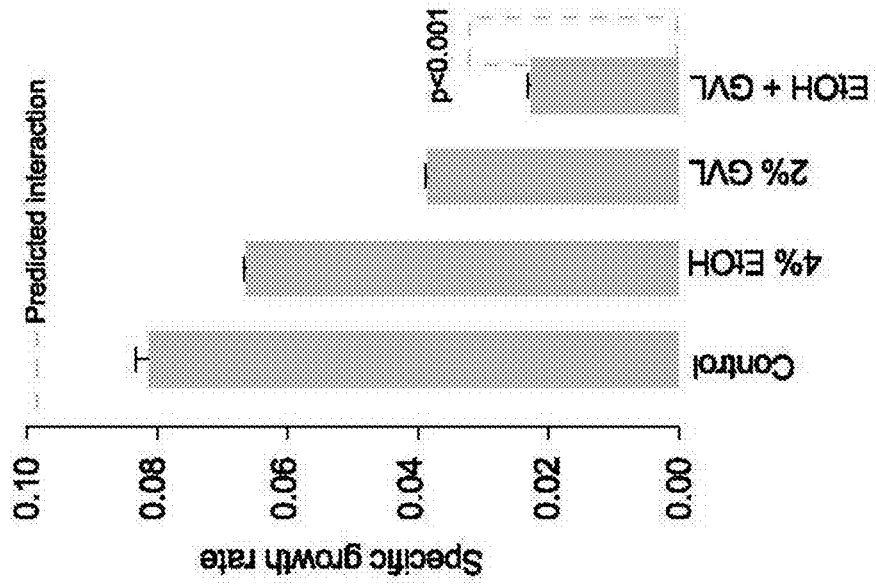


FIGS. 3A-3C

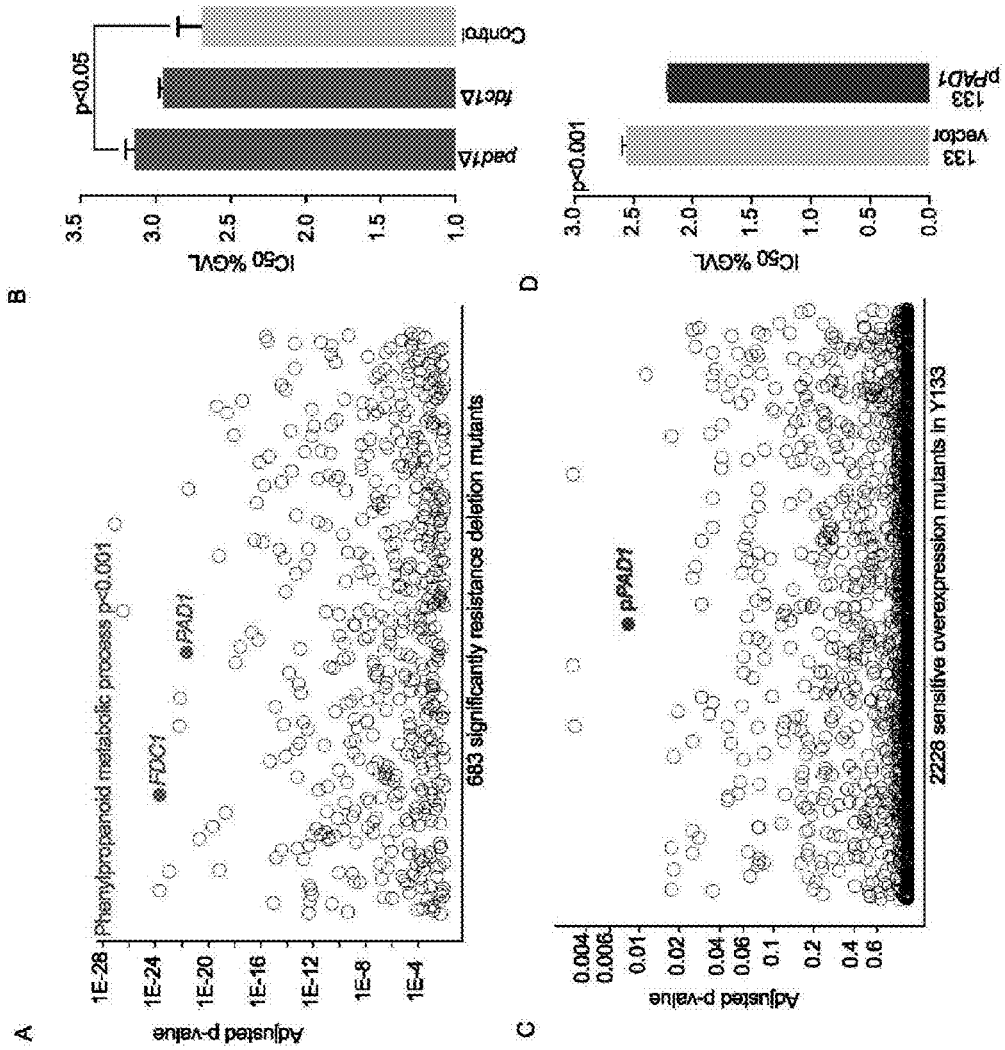


FIGS. 3A-3C, CONTINUED

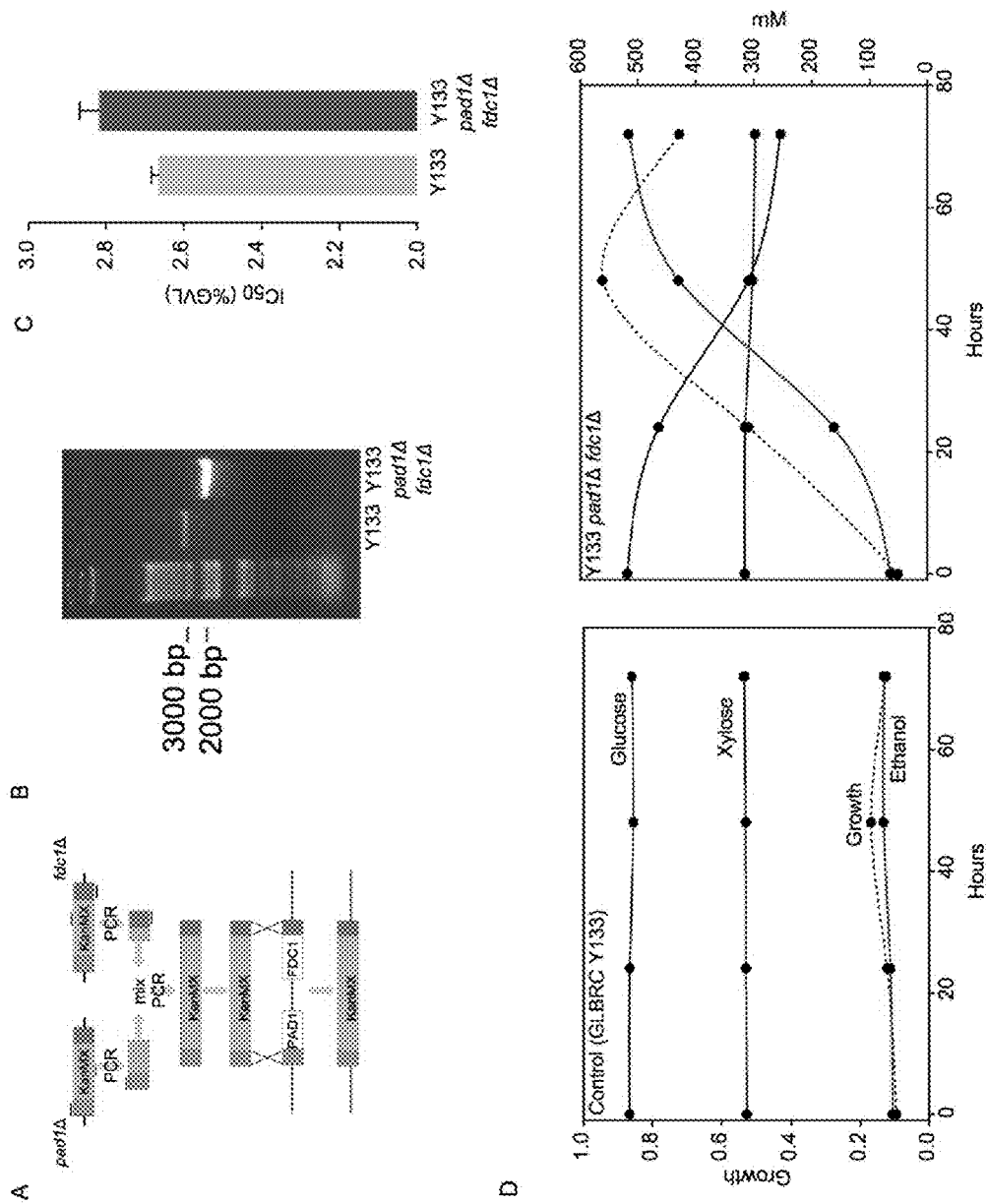
C



FIGS. 4A-4D

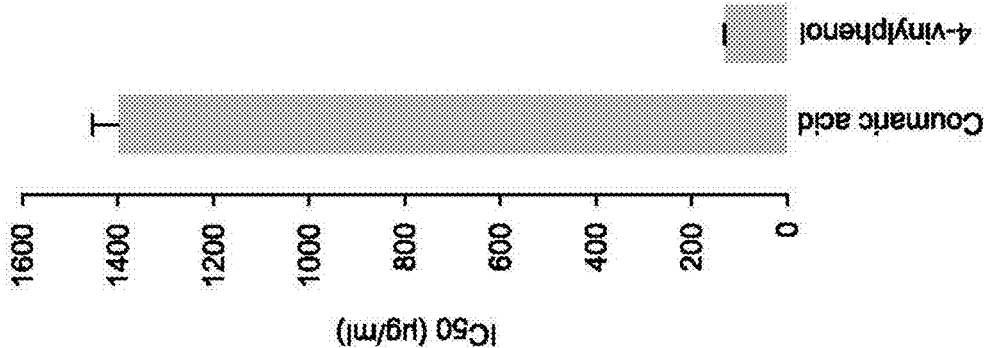


FIGS. 5A-5D

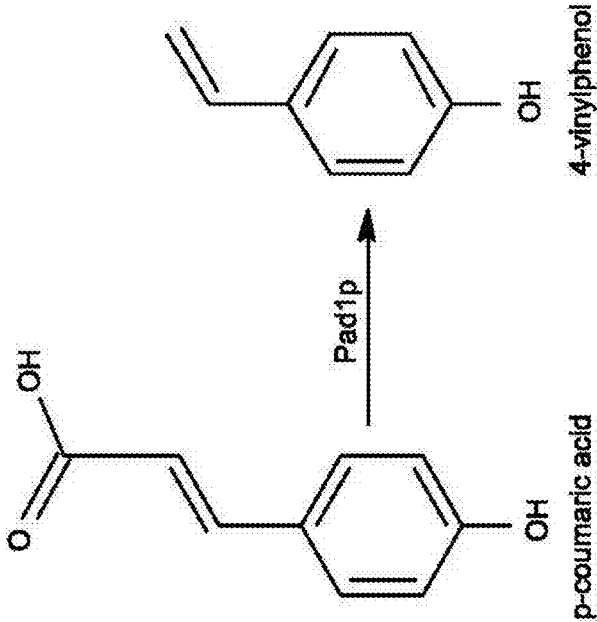


FIGS. 6A-6D

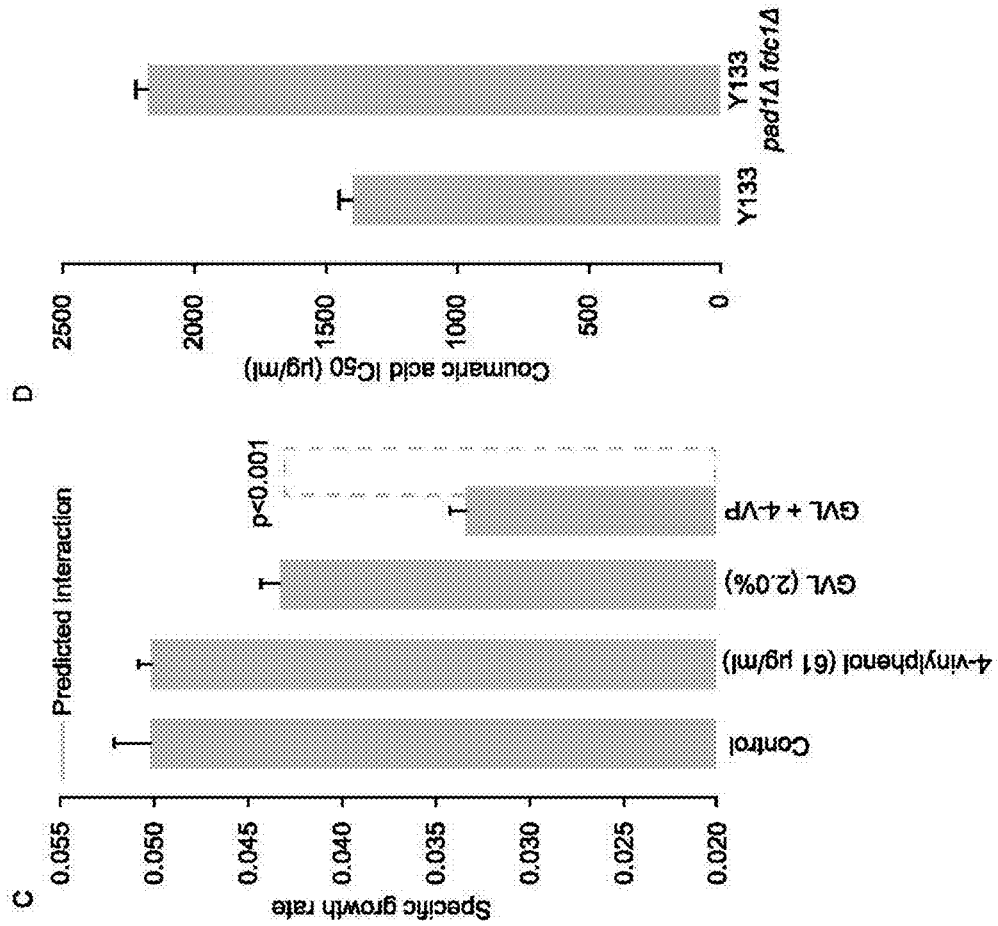
B



A



FIGS. 6A-6D, CONTINUED



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**RECOMBINANT YEAST HAVING
ENHANCED GAMMA VALEROLACTONE
TOLERANCE AND METHODS OF USE**

CROSS-REFERENCE TO RELATED
APPLICATIONS

This application claims the benefit of U.S. Provisional Patent Application No. 62/048,458, filed Sep. 10, 2014; which is incorporated herein by reference as if set forth in its entirety.

STATEMENT REGARDING FEDERALLY
SPONSORED RESEARCH OR DEVELOPMENT

This invention was made with government support under DE-FC02-07ER64494 awarded by the U.S. Department of Energy. The government has certain rights in the invention.

FIELD OF THE INVENTION

Broadly, the present invention relates to materials and methods for the production of ethanol. In particular, the present invention relates to genetically modified yeast strains useful for glucose and xylose fermentation and, more specifically, to strains of *Saccharomyces cerevisiae* genetically engineered for enhanced tolerance for gamma valerolactone (GVL) toxicity and methods of using the same for improved GVL-mediated hydrolysis of lignocellulosic biomass for industrial-scale ethanol production.

BACKGROUND

Cellulosic biomass is a vast source of renewable energy and an abundant substrate for biofuel production. As an alternative to corn-based ethanol, bioethanol can be generated from lignocellulosic (LC) sugars derived from cellulosic biomass of renewable and sustainable plant feedstocks. Energy of cellulosic biomass is primarily stored as the recalcitrant polysaccharide cellulose, which is difficult to hydrolyze because of the highly crystalline structure, and in hemicellulose, which presents challenges because of its structural diversity and complexity. Many microbes cannot natively ferment pentose sugars (e.g., xylose) from complex lignocellulosic biomass, which is composed of cellulose, hemicellulose and lignin fractions. Even when engineered to express the minimal enzymes from native pentose sugar-metabolizing organisms, *S. cerevisiae* cannot ferment xylose from innocuous lab media at industrially-acceptable rates. Lalue et al., *Applied Microbiol. Biotech.* 166:1908 (2012); Almeida et al., *Biotech. J.* 6:286 (2011). Xylose is a prevalent sugar in both woody and herbaceous plants and a major component of hemicelluloses. Bioconversion of both xylose and glucose is required for the production of cellulosic biofuels. To further complicate matters, plant biomass must be chemically, mechanically, or thermally pretreated prior to enzymatic hydrolysis ex situ in order to produce fermentable glucose and xylose monomers. Such pretreatment processes generate a diverse array of degradation products derived from plant cell walls, such as hemicellulose and lignin-derived acetate and aromatic molecules, many of which inhibit cellular metabolism in *S. cerevisiae* and induce microbial stress during hydrolysate fermentation. Taylor et al., *Biotechnology J.* 7:1169 (2012); Liu, *Applied Microbiol. Biotech.* 90:809 (2011). At present, little is known about how such inhibitors impact xylose fermentation, particularly

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under strict industrially relevant, anaerobic conditions where ethanol production is maximized.

In view of the current state of the biofuel industry, particularly ethanol production based on glucose- and xylose-containing feedstocks, it can be appreciated that there remains a need for efficient and cost-effective processes for breaking down cellulose and hemicellulose into their constituent sugars.

SUMMARY OF THE INVENTION

The present invention is largely related the inventors' research efforts to better understand xylose utilization for microbial engineering. The invention relates generally to methods and compositions for digesting lignocellulosic material and more particularly to methods that involve exposing the material to genetically engineered *Saccharomyces cerevisiae* (*S. cerevisiae*) variants having enhanced tolerance for or resistance to gamma valerolactone (GVL)-mediated toxicity.

In a first aspect, provided herein is a recombinant yeast that has been genetically engineered to exhibit a reduced amount of functional PAD1 polypeptide. The recombinant yeast has increased tolerance to gamma valerolactone (GVL) toxicity relative to a wild-type yeast or another recombinant yeast not exhibiting a reduced amount of functional PAD1 polypeptide. The recombinant yeast can further exhibit a reduced amount of functional FDC1 polypeptide, wherein the recombinant yeast has increased tolerance to gamma valerolactone (GVL) toxicity relative to a wild-type yeast or another recombinant yeast not exhibiting reduced amounts of functional PAD1 and FDC1 polypeptides. In some cases, a recombinant yeast comprises a disabling mutation in a gene encoding PAD1 polypeptide. The recombinant yeast can further comprise a disabling mutation in a gene encoding FDC1 polypeptide. The gene encoding PAD1 polypeptide can be SEQ ID NO:8. The gene encoding FDC1 polypeptide can be SEQ ID NO:10.

In some cases, a recombinant yeast further exhibits reduced or undetectable amounts of functional ISU1, GRE3, and IRA2 polypeptides, wherein the recombinant yeast is capable of increased aerobic or anaerobic xylose fermentation relative to a wild-type yeast or another recombinant yeast not exhibiting reduced amounts of functional PAD1, ISU1, GRE3, and IRA2 polypeptides. The recombinant yeast can have disabling mutation at each of loci *isu1*, *gre3*, and *ira2*, whereby the mutations result in reduced amounts of functional ISU1, GRE3, and IRA2 polypeptides, respectively. The disabling mutation at the *gre3* locus can comprise a substitution of a threonine for the alanine at amino acid residue position 46 of SEQ ID NO:4. The disabling mutation at the *ira2* locus can comprise a substitution of a stop codon for the glutamate at amino acid residue at position 2927 of SEQ ID NO:2. The disabling mutation at the *isu1* locus can comprise a substitution of a tyrosine for the histidine at amino acid residue position 138 of SEQ ID NO:6. The recombinant yeast can produce ethanol at an increased rate relative to a wild-type yeast or another recombinant yeast not exhibiting reduced or undetectable amounts of functional ISU1, GRE3, and IRA2 polypeptides. The increased rate of ethanol production can occur under anaerobic conditions. The recombinant yeast can be of the genus *Saccharomyces*. The recombinant yeast can be of the species *Saccharomyces cerevisiae*. A portion of an extrachromosomal vector stably maintained in the recombinant yeast can comprise the disabling mutation. A nucleic acid sequence

comprising the disabling mutation can be integrated into a chromosome of the recombinant yeast.

In another aspect, a yeast inoculum is provided herein. The yeast inoculum can comprise a recombinant yeast as described herein and a culture medium.

In a further aspect of the invention, a method for fermenting cellulosic material into ethanol is provided. The method comprises contacting a GVL-treated hydrolysate to a recombinant yeast or a yeast inoculum provided herein for a period of time sufficient to allow fermentation of at least a portion of the cellulosic material to ethanol, whereby the rate of fermentation of cellulosic material of the GVL-treated hydrolysate to ethanol is increased relative to the fermentation rate of a GVL-treated hydrolysate not contacted to the recombinant yeast or the yeast inoculum. The method can further comprise separating the ethanol from fermented cellulosic material. The GVL-treated hydrolysate can comprise xylose. The recombinant yeast can be *Saccharomyces cerevisiae*. The cellulosic material can comprise lignocellulosic biomass. In some cases, the lignocellulosic biomass comprises at least one material selected from the group consisting of agricultural residues, wood, municipal solid wastes, paper and pulp industry wastes, and herbaceous crops.

These and other features, objects, and advantages of the present invention will become better understood from the description that follows. In the description, reference is made to the accompanying drawings, which form a part hereof and in which there is shown by way of illustration, not limitation, embodiments of the invention. The description of preferred embodiments is not intended to limit the invention to cover all modifications, equivalents and alternatives. Reference should therefore be made to the claims recited herein for interpreting the scope of the invention.

BRIEF DESCRIPTION OF THE DRAWINGS

The present invention will be better understood and features, aspects and advantages other than those set forth above will become apparent when consideration is given to the following detailed description thereof. Such detailed description makes reference to the following drawings, wherein:

FIGS. 1A-1B show production of GVL hydrolysates and relative toxicity. Lignocellulosic biomass is heated with GVL to convert the cellulose and hemicellulose to sugar monomers, the result is a hydrolysate of sugars, amino acids, lignocellulosic derived fermentation inhibitors, and residual GVL that cannot be recovered (~1-3%) (A). The half-maximal inhibitory concentration (IC₅₀) of GVL in rich media is 2.7% (B).

FIGS. 2A-2C show chemical genomic profiling of GVL. Chemical genomic profiling (A) revealed a significant enrichment for genes involved in late endosome to vacuole (p<0.01) among the top gene mutants sensitive to GVL (B). Single mutant validations of these individual mutants confirmed they were significantly more sensitive to GVL (C). (Mean±S.E., n=3).

FIGS. 3A-3C demonstrate that GVL rapidly compromises membrane integrity and is synergistic with ethanol. GVL compromises membrane integrity as determined by dye uptake after treatment, and this effects is apparent with as little as 2.5% GVL (A, B). GVL is significantly synergistic with ethanol (C). (Mean±S.E., n=3).

FIGS. 4A-4D present genes mediating GVL toxicity by deletion and overexpression mutant profiling. Among deletion mutants significantly resistant to GVL, we saw signifi-

cant enrichment for genes in phenylpropanoid metabolism (p<0.001), driven by the mutants of the decarboxylases Pad1p and Fdc1p (A). Individual mutants in these genes were more tolerant of GVL (B). Overexpression profiling using MoBY-ORF transformed Y133 demonstrated that overexpression of PAD1 conferred significant GVL sensitivity (C). Increased expression of PAD1 significantly reduced GVL tolerance in single mutant cultures (D). (Mean±S.E., n=3).

FIGS. 5A-5D demonstrate that deletion of PAD1 and FDC1 confers tolerance of GVL in a xylose fermenting yeast. A two-step PCR approach was used to simultaneously delete PAD1 and FDC1 in Y133, which are adjacent on chromosome IV (A), and confirmed deletion by PCR (B). The Y133 pad1Δfdc1Δ mutant had significantly greater (p<0.01) tolerance of GVL (C), and also had faster growth, sugar consumption, and ethanol production under anaerobic conditions in synthetic hydrolysate with 1% GVL (D).

FIGS. 6A-6D demonstrate that vinyl products of PAD1 and FDC1 are more toxic than the acid precursors, and are synergistic with GVL. The decarboxylase Pad1p converts phenolic acids to a vinyl form (A). The vinyl derivative of coumaric acid (4-vinylphenol) is significantly more toxic than the acid form (B, p<0.001). 4-vinylphenol is significantly synergistic with GVL (C). Deletion of PAD1 and FDC1 confers resistance to coumaric acid (D).

While the present invention is susceptible to various modifications and alternative forms, exemplary embodiments thereof are shown by way of example in the drawings and are herein described in detail. It should be understood, however, that the description of exemplary embodiments is not intended to limit the invention to the particular forms disclosed, but on the contrary, the intention is to cover all modifications, equivalents and alternatives falling within the spirit and scope of the invention as defined by the appended claims.

DETAILED DESCRIPTION OF THE INVENTION

In General

Before the present materials and methods are described, it is understood that this invention is not limited to the particular methodology, protocols, materials, and reagents described, as these may vary. It is also to be understood that the terminology used herein is for the purpose of describing particular embodiments only, and is not intended to limit the scope of the present invention, which will be limited only by the appended claims.

It must be noted that as used herein and in the appended claims, the singular forms "a," "an," and "the" include plural reference unless the context clearly dictates otherwise. As well, the terms "a" (or "an"), "one or more" and "at least one" can be used interchangeably herein. It is also to be noted that the terms "comprising," "including," and "having" can be used interchangeably.

Unless defined otherwise, all technical and scientific terms used herein have the same meanings as commonly understood by one of ordinary skill in the art to which this invention belongs. Although any methods and materials similar or equivalent to those described herein can be used in the practice or testing of the present invention, the preferred methods and materials are now described. All publications and patents specifically mentioned herein are incorporated by reference for all purposes including describing and disclosing the chemicals, cell lines, vectors, animals, instruments, statistical analysis and methodologies which

are reported in the publications which might be used in connection with the invention. All references cited in this specification are to be taken as indicative of the level of skill in the art. Nothing herein is to be construed as an admission that the invention is not entitled to antedate such disclosure by virtue of prior invention.

The practice of the present invention will employ, unless otherwise indicated, conventional techniques of molecular biology, microbiology, recombinant DNA, and immunology, which are within the skill of the art. Such techniques are explained fully in the literature. See, for example, *Molecular Cloning A Laboratory Manual*, 2nd Ed., ed. by Sambrook, Fritsch and Maniatis (Cold Spring Harbor Laboratory Press: 1989); *DNA Cloning*, Volumes I and II (D. N. Glover ed., 1985); *Oligonucleotide Synthesis* (M. J. Gait ed., 1984); Mullis et al. U.S. Pat. No. 4,683,195; *Nucleic Acid Hybridization* (B. D. Hames & S. J. Higgins eds. 1984); *Transcription And Translation* (B. D. Hames & S. J. Higgins eds. 1984); *Culture Of Animal Cells* (R. I. Freshney, Alan R. Liss, Inc., 1987); *Immobilized Cells And Enzymes* (IRL Press, 1986); B. Perbal, *A Practical Guide To Molecular Cloning* (1984); the treatise, *Methods In Enzymology* (Academic Press, Inc., N.Y.); *Gene Transfer Vectors For Mammalian Cells* (J. H. Miller and M. P. Calos eds., 1987, Cold Spring Harbor Laboratory); *Methods In Enzymology*, Vols. 154 and 155 (Wu et al. eds.), *Immunochemical Methods In Cell And Molecular Biology* (Mayer and Walker, eds., Academic Press, London, 1987); and *Handbook Of Experimental Immunology*, Volumes I-IV (D. M. Weir and C. C. Blackwell, eds., 1986).

The nucleotides which occur in the various nucleotide sequences appearing herein have their usual single-letter designations (A, G, T, C or U) used routinely in the art. In the present specification and claims, references to Greek letters may either be written out as alpha, beta, etc. or the corresponding Greek letter symbols (e.g., α , β , etc.) may sometimes be used.

As used herein, the term polynucleotide generally refers to any polyribonucleotide or polydeoxyribonucleotide, which may be unmodified RNA or DNA or modified RNA or DNA. Polynucleotides include, without limitation, single- and double-stranded DNA, DNA that is a mixture of single- and double-stranded regions or single-, double- and triple-stranded regions, single- and double-stranded RNA, and RNA that is mixture of single- and double-stranded regions, hybrid molecules comprising DNA and RNA that may be single-stranded or, more typically, double-stranded, or triple-stranded regions, or a mixture of single- and double-stranded regions. As used herein, the term polynucleotide also includes DNAs or RNAs as described above that contain one or more modified bases. Thus, DNAs or RNAs with backbones modified for stability or for other reasons are "polynucleotide(s)" as that term is intended herein. Moreover, DNAs or RNAs comprising unusual bases, such as inosine, or modified bases, such as tritylated bases, to name just two examples, are polynucleotides as the term is used herein. It will be appreciated that a great variety of modifications have been made to DNA and RNA that serve many useful purposes known to those of skill in the art. The term polynucleotide as it is employed herein embraces such chemically, enzymatically or metabolically modified forms of polynucleotides, as well as the chemical forms of DNA and RNA characteristic of viruses and cells, including, for example, simple and complex cells. The term polynucleotide also embraces short polynucleotides often referred to as oligonucleotide(s).

The term "isolated nucleic acid" as used herein means a nucleic acid isolated from its natural environment or prepared using synthetic methods such as those known to one of ordinary skill in the art. Complete purification is not required in either case. The nucleic acids of the invention can be isolated and purified from normally associated material in conventional ways such that in the purified preparation the nucleic acid is the predominant species in the preparation. At the very least, the degree of purification is such that the extraneous material in the preparation does not interfere with use of the nucleic acid of the invention in the manner disclosed herein. The nucleic acid is preferably at least about 85% pure, more preferably at least about 95% pure and most preferably at least about 99% pure.

Further, an isolated nucleic acid has a structure that is not identical to that of any naturally occurring nucleic acid or to that of any fragment of a naturally occurring genomic nucleic acid spanning more than three separate genes. An isolated nucleic acid also includes, without limitation, (a) a nucleic acid having a sequence of a naturally occurring genomic or extrachromosomal nucleic acid molecule but which is not flanked by the coding sequences that flank the sequence in its natural position; (b) a nucleic acid incorporated into a vector or into a prokaryote or eukaryote genome such that the resulting molecule is not identical to any naturally occurring vector or genomic DNA; (c) a separate molecule such as a cDNA, a genomic fragment, a fragment produced by polymerase chain reaction (PCR), or a restriction fragment; and (d) a recombinant nucleotide sequence that is part of a hybrid gene. Specifically excluded from this definition are nucleic acids present in mixtures of clones, e.g., as those occurring in a DNA library such as a cDNA or genomic DNA library. An isolated nucleic acid can be modified or unmodified DNA or RNA, whether fully or partially single-stranded or double-stranded or even triple-stranded. A nucleic acid can be chemically or enzymatically modified and can include so-called non-standard bases such as inosine, as described in a preceding definition.

Compositions of the Invention

Efficient biochemical conversion and fermentation of renewable lignocellulosic feedstocks is essential for the production of biofuels and other bioproducts from plant materials. While *S. cerevisiae* excel at fermentation of glucose from corn and sugar cane, the fermentation of renewable lignocellulosic biomass presents a significant challenge. Xylose, which is a pentose sugar and a major component of hemicellulose, can comprise almost 30% of total cell wall carbohydrate in grasses. Its conversion, along with glucose, into ethanol is critical for any economically-viable cellulosic biofuel process. Biomass pretreatments and enzymatic hydrolysis are viable but costly ways of depolymerizing cellulose and hemicellulose fractions of biomass to produce soluble carbohydrates. Large-scale depolymerization cellulose and hemicellulose fractions of biomass is increasingly economically feasible as the cost of pretreatment reagents drops. Acid-catalyzed hydrolysis methods are generally less expensive than enzyme-catalyzed methods. Gamma-valerolactone (GVL) is an inexpensive solvent that can be derived from cellulose or hemicelluloses. GVL promotes thermocatalytic saccharification through complete solubilization of all lignocellulosic biomass components including lignin, which makes GVL-mediated hydrolysis of lignocellulosic biomass a potentially transformative technology for biofuel production. Luterbacher et al., *Science* 343:277-280 (2014); see also Bond et al., *Integrated Catalytic Conversion of γ -Valerolactone to Liquid Alkenes for Transportation Fuels*, *Science* 26: (2010). Standard methods

of GVL-mediated hydrosylation yields hydrolysates having high sugar levels (glucose and xylose) but also having residual levels of GVL that are toxic to fermentative microorganisms such as yeast. Current GVL-mediated hydrolysis methods yield hydrolysates comprising about 2.3% residual GVL. The present invention is based, at least in part, on the Inventors' discovery of genetic modifications that increase a yeast strain's tolerance for GVL toxicity and increase its growth rate in the presence of GVL.

Accordingly, one aspect of the present invention relates to eukaryotic host cells genetically engineered for improved tolerance to GVL toxicity. In particular, the present invention provides eukaryotic cells that have been genetically engineered to have enhanced GVL toxicity tolerance, enhanced anaerobic and/or aerobic xylose fermentation, and increased ethanol production relative to an unmodified cell or a recombinant cell not genetically engineered as described herein. Modified cells of the present invention are well-suited for producing a variety of fermentation products, including ethanol, in fermentation processes that use xylose or a combination of xylose and glucose as carbon sources.

As used herein, a "host cell" is a cell which has been transformed or transfected, or is capable of transformation or transfection by an exogenous polynucleotide sequence. A host cell that has been transformed or transfected may be more specifically referred to as a "recombinant host cell." A preferred host cell is a host cell that is naturally capable of alcoholic fermentation, preferably, anaerobic alcoholic fermentation. Host cells may also exhibit a high tolerance to ethanol, low pH, organic acids, and/or elevated temperatures. Such characteristics or activities of the host cell may be naturally present in the host cell or may be introduced or modified by genetic modification. Preferred host cells for the present invention include yeast cells, particularly yeast cells of the genus *Saccharomyces*. Preferred yeast species as host cells include *Saccharomyces cerevisiae*, *S. bulderi*, *S. barnettii*, *S. exiguus*, *S. uvarum*, *S. diastaticus*, *K. lactis*, *K. marxianus*, and *K. fragilis*, of which yeast cells of the genus *Saccharomyces* and yeast cells of the species *Saccharomyces cerevisiae* (*S. cerevisiae*) are preferred. Yeasts of the genus *Saccharomyces* possess both a metabolic pathway and a fermentative pathway for respiration.

"Yeasts" are eukaryotic micro-organisms classified in the kingdom Fungi. Most reproduce asexually by budding, although some yeasts undergo sexual reproduction by meiosis. Yeasts are unicellular, although some species with yeast forms may become multi-cellular through the formation of a string of connected budding cells known as pseudohyphae, or false hyphae, as seen in most molds. Yeasts do not form a single taxonomic or phylogenetic grouping. The term "yeast" is often taken as a synonym for *Saccharomyces cerevisiae*, but the phylogenetic diversity of yeasts is illustrated by their assignment to two taxonomic classes of fungi, the ascomycetes and the basidiomycetes.

In exemplary embodiments, a genetically modified yeast of the present invention comprises one or more genetic modifications that reduce or disrupt expression of functional PAD1 (phenylacrylic acid decarboxylase) polypeptide or functional FDC1 (ferulic acid decarboxylase) polypeptide. PAD1 and FDC1 are phenylacrylic acid decarboxylases that decarboxylate aromatic phenylacrylic acids (e.g., ferulic acid, p-coumaric acid, cinnamic acid) in *S. cerevisiae*. See Clausen et al., *Gene* 142(1):107-12 (1994); Mukai et al., *J. Bioscience & Bioengineering* 109(6):564-569 (2010). Full-length PAD1 (NCBI Gene ID: 852150) polypeptide is 242 amino acids. Full-length FDC1 (NCBI Gene ID: 852152) polypeptide is 503 amino acids. By "delete or disrupt", it is

meant that the entire coding region of the gene is eliminated (deletion), or the gene or its promoter and/or terminator region is modified (such as by deletion, insertion, or mutation) such that the gene no longer produces a partially or fully non-functional polypeptide (i.e., lacking enzymatic activity), or produces an enzyme with severely reduced activity. The deletion or disruption can be accomplished by genetic engineering methods, forced evolution or mutagenesis, and/or selection or screening.

In some cases, a recombinant yeast of the present invention comprises a genetic modification that deletes or disrupts a Pad1 nucleic acid that encodes PAD1 polypeptide, whereby the genetically modified yeast produces a reduced level of functional PAD1 polypeptide. In some cases, such genetically modified yeast produce no or substantially no functional PAD1 polypeptide. In other embodiments, a recombinant yeast of the present invention comprises a genetic modification that deletes or disrupts a Fdc1 nucleic acid that encodes FDC1 polypeptide, whereby the genetically modified yeast produces a reduced level of functional FDC1 polypeptide. In some cases, such a genetically modified yeast produces no or substantially no functional PAD1 polypeptide. In some cases, it will be advantageous to genetically modify a host cell to comprise genetic modifications that cause reduced levels of both functional polypeptides, PAD1 and FDC1. Recombinant yeast comprising one or more of the genetic modifications described herein exhibit improved fermentation rates relative to unmodified yeast or yeast not comprising the genetic modifications described herein. Such recombinant yeast also exhibit increased tolerance to GVL toxicity and improved growth rates in hydrolysates comprising residual GVL following GVL-mediated hydrolysis.

It is contemplated that certain additional genetic modifications may be advantageous or necessary to produce other desirable characteristics and/or to enable the yeast cell to produce certain products at industrially-acceptable levels. For example, genetic modifications that reduce or eliminate functional PAD1 polypeptide or functional FDC1 polypeptide can be introduced into *S. cerevisiae* yeast of the GLBRCY133 ("Y133") strain (a GLBRCY128 derivative). Yeast of the GLBRCY128 ("Y128") strain were evolved for robust, anaerobic xylose metabolism under industrially relevant conditions and high yields of extracellular ethanol. Forced evolution of the Y128 yeast strain from a background strain designated NRRL YB-210/GLBRCY0 (Mortimer and Johnston, *Genetics* 113(1):35-43 (1986)), has been described elsewhere. See U.S. Application No. 61/978,585, filed Apr. 11, 2014. Yeast of the Y133 strain comprise the genotype of GLBRCY128, but with the loxP-KanMX-loxP marker excised by Cre as previously described (Parreiras et al., *PLoS One*. 2014; 9(9):e107499).

Accordingly, in some cases, a recombinant yeast of the present invention comprises a genetic modification that deletes or disrupts a Pad1 nucleic acid that encodes PAD1 polypeptide and further comprises a disabling mutation at each of loci *isu1*, *gre3*, and *ira2*, whereby the mutations result in reduced amounts of functional ISU1, GRE3, and IRA2 polypeptides.

The degree of GVL's toxicity to a microorganism such as yeast depends on the yeast's growth conditions. Generally, yeast grown in a minimal medium are more sensitive to chemical stress, while yeast grown in a nutrient-rich medium are more tolerant of chemical stress. Recombinant yeast of the present invention tolerate higher levels of GVL relative to a wild type yeast or yeast not comprising a genetic modification described herein when grown in either a nutri-

ent-rich medium or minimal medium. In exemplary embodiments, a recombinant yeast of the present invention that comprises a genetic modification resulting in reduced levels of functional PAD1 polypeptide has significantly more GVL tolerance ($P < 0.05$) than a yeast having the same genetic background but having normal levels of functional PAD1 polypeptide, even when growth under industrially relevant conditions in a minimal medium with high sugar loading (osmotically stressful). In general, toxicity is expressed as the “half maximal inhibitory concentration” or “IC₅₀.” The terms “half maximal inhibitory concentration” and “IC₅₀” are used interchangeably and, as used herein, refer to a concentration of the compound that is required to inhibit a given biological or biochemical function by half. In a standard yeast lab strain, the IC₅₀ is about 1.98% GVL, while a PAD1 deletion mutant in the standard lab strain background has an IC₅₀ of about 2.4% GVL and FDC1 deletion mutant in the standard lab strain background has an IC₅₀ of about 2.1% GVL. In other words, a yeast having a genetic modification (in a standard lab strain background) that eliminates functional PAD1 polypeptide can tolerate GVL toxicity wherein GVL comprises about 2.4% of the hydrosylate. Similarly, yeast having a genetic modification (in a standard lab strain background) that eliminates functional FDC1 polypeptide can tolerate GVL toxicity wherein GVL comprises about 2.1% of the hydrosylate.

The GVL IC₅₀ for a genetically modified yeast of the present invention, when grown anaerobically in a minimal medium, is in the range between about 1.15% GVL and about 1.28% GVL, as compared to an IC₅₀ of about 1.0% for unmodified yeast of the xylose-fermenting background strain (Y128). When grown in a nutrient-rich media, yeast of the Y128 xylose-fermenting strain have an IC₅₀ of about 2.2% GVL, whereas genetically modified yeast of the present invention have an IC₅₀ of about 2.4% GVL to about 2.5% GVL. When grown in a nutrient-rich media, yeast of the Y133 xylose-fermenting strain have an IC₅₀ of about 2.7% GVL, whereas yeast of the genetically modified strain (e.g., Y133 pad1Δfdc1Δ) of the present invention has an IC₅₀ of about 2.9% GVL.

In some cases, a suitable host yeast cell comprises at least one native gene (a “xylose isomerase gene”) that produces an active xylose isomerase enzyme that is capable of catalyzing the interconversion of D-xylose to D-xylulose. Xylose isomerase can also catalyze the interconversion of D-ribose to D-ribulose and D-glucose to D-fructose. The enzyme can be specific to the reduction of xylose or non-specific (i.e., capable of catalyzing the conversion of a range of pentose sugars). In some cases, a suitable host yeast cell is genetically engineered to contain an expression cassette containing *Clostridium phytofermentans* xylose isomerase (CphytoXylA), which can confer anaerobic xylose fermentation by *S. cerevisiae* with additional genetic modifications (see Brat et al., *Applied Environmental Microbiol.* 75:2304 (2009)), driven by the ScerTDH3 promoter. In exemplary embodiments, the expression cassette further comprises ScerTAL1, a Pentose Phosphate Pathway transaldolase enzyme that can improve xylose metabolism when overexpressed (see Ni et al., *Applied Environmental Microbiol.* 73:2061 (2007); Walfridsson et al., *Applied Environmental Microbiol.* 61:4184 (1995)), and SstipXYL3 driven by the ScerPGK1 and ScerTEF2 promoters, respectively. For example, the host yeast cell can comprise a TAL1-XylA-XYL3 gene expression cassette.

Genetic modification of the host cell can be accomplished in one or more steps via the design and construction of appropriate vectors and transformation of the host cell with

those vectors. Nucleic acid constructs useful in the invention may be prepared in conventional ways, by isolating the desired genes from an appropriate host, by synthesizing all or a portion of the genes, or combinations thereof. Similarly, the regulatory signals, the transcriptional and translational initiation and termination regions, may be isolated from a natural source, be synthesized, or combinations thereof. The various fragments may be subjected to endonuclease digestion (restriction), ligation, sequencing, in vitro mutagenesis, primer repair, or the like. The various manipulations are well known in the literature and will be employed to achieve specific purposes.

The various nucleic acids and/or fragments thereof may be combined, cloned, isolated and sequenced in accordance with conventional ways. After each manipulation, the DNA fragment or combination of fragments may be inserted into the cloning vector, the vector transformed into a cloning host, e.g., *E. coli*, the cloning host grown up, lysed, the plasmid isolated and the fragment analyzed by restriction analysis, sequencing, combinations thereof, or the like.

Targeted integration can be accomplished by designing a vector having regions that are homologous to the upstream (5'-) and downstream (3'-) flanks of the target gene. Either of both of these regions may include a portion of the coding region of the target gene. The gene cassette (including associated promoters and terminators if different from those of the target gene) and selection markers (with associated promoters and terminators as may be needed) can reside on a vector between the regions that are homologous to the upstream and downstream flanks of the target gene. Targeted cassette insertion can be verified by any appropriate method such as, for example, PCR. A host cell may be transformed according to conventional methods that are known to practitioners in the art. Electroporation and/or chemical (such as calcium chloride- or lithium acetate-based) transformation methods can be used. The DNA used in the transformations can either be cut with particular restriction enzymes or used as circular DNA. Methods for transforming yeast strains are described in WO 99/14335, WO 00/71738, WO 02/42471, WO 03/102201, WO 03/102152 and WO 03/049525; these methods are generally applicable for transforming host cells in accordance with this invention. Other methods for transforming eukaryotic host cells are well known in the art such as from standard handbooks, such as Sambrook and Russel (2001) “Molecular Cloning: A Laboratory Manual (3rd edition),” Cold Spring Harbor Laboratory, Cold Spring Harbor Laboratory Press, or F. Ausubel et al., eds., “Current protocols in molecular biology,” Green Publishing and Wiley Interscience, New York (1987).

In another aspect, compositions of the present invention further include yeast inocula comprising recombinant yeast as provided herein. A yeast inoculum of the present invention comprises (a) a recombinant yeast as provided herein and (b) a culture medium. In exemplary embodiments, the recombinant yeast is *S. cerevisiae* and the culture medium is a liquid culture medium. Yeast inocula of the present invention include large-scale preparations of sufficient quantities of viable yeast cells for use in, for example, xylose fermentation and other industrial ethanol-producing methods. When contacted to a GVL-treated hydrosylate comprising some level of residual GVL, a yeast inoculum of the present invention exhibits improved xylose fermentation rates and increased growth rates relative to a yeast inoculum that does not comprise a recombinant yeast of the present invention.

Methods of the Invention

The methods provided by the present invention involve the discovery and incorporation of genetic modifications

into genes encoding certain polypeptides into a single host organism and the use of those organisms to convert xylose to ethanol. In particular, the present invention provides a method of fermenting cellulosic material comprising the 5-carbon sugar xylose into ethanol, where the method comprises use of a recombinant yeast having enhanced tolerance of GVL relative to wild type yeast or a recombinant yeast not comprising the genetic modifications described herein.

In exemplary embodiments, recombinant yeast of the present invention are used to make ethanol by converting xylose and other sugars under appropriate fermentation conditions. The sugars can come from a variety of sources including, but not limited to, cellulosic material. The cellulosic material can be lignocellulosic biomass. As used herein, the term "lignocellulosic biomass" refers to any materials comprising cellulose, hemicellulose, and lignin, wherein the carbohydrate polymers (cellulose and hemicelluloses) are tightly bound to the lignin. Generally, lignocellulosic material for making ethanol is feedstock such as corn stover, which consists of the stems, cobs, and leaves from the corn plants (i.e., the non-grain material). Corn stover is typically shredded by mechanical means and incorporated by tillage into topsoil for decomposition. In addition to lignocellulosic ethanol production from corn stover, other feedstocks such as sorghum, wheat, or another grain can be used. In some cases, lignocellulosic biomass comprises material selected from the group consisting of materials that comprise at least 75% cellulose, cellulose/hemicelluloses, xylose, biomass, and chitin. In other cases, the lignocellulosic biomass comprises at least one material selected from the group consisting of agricultural residues, wood, municipal solid wastes, paper and pulp industry wastes, and herbaceous crops. As used herein, the term "biomass" refers to a renewable energy source, is biological material from living or recently living organisms. As an energy source, biomass can either be used directly, or converted into other energy products such as biofuel. Biomass includes plant or animal matter that can be converted into fibers or other industrial chemicals, including biofuels. Industrial biomass can be grown from numerous types of plants, including miscanthus, switchgrass, hemp, corn, poplar, willow, sorghum, sugarcane, bamboo, and a variety of tree species, ranging from eucalyptus to oil palm (palm oil). Thus, biomass can include wood biomass and non-wood biomass.

In some cases, methods of the present invention include a hydrolyzation step. For example, when cellulosic material is used in the methods disclosed herein, the material can be hydrolyzed to produce a hydrolysate comprising xylose and glucose, which is subsequently contacted to one or more recombinant yeasts of the present invention. As used herein, the term "hydrolysate" refers to a fermentable sugar-containing product produced from cellulosic material (e.g., biomass), typically through pretreatment and saccharification processes. In exemplary embodiments, cellulosic material is pretreated using a solvent comprising gamma-valerolactone (GVL or γ -valerolactone). Such a pretreatment may also comprise one or more physical or chemical treatments such as grinding, milling, cutting, base treatment such as with ammonia or NaOH, and acid treatment.

In some cases, GVL-mediated hydrolysis further comprises an enzymatic saccharification treatment. Enzymatic saccharification typically makes use of an enzyme composition or blend to break down cellulose and/or hemicellulose and to produce a GVL-treated hydrolysate containing 6-carbon sugars (e.g., glucose) and 5-carbon sugars (e.g., xylose, arabinose) For review of saccharification enzymes, see Lynd et al., *Microbiol. Mol. Biol. Rev.* 66:506-577 (2002). Sac-

charification enzymes may be obtained commercially. In some cases, saccharification enzymes may be produced using recombinant microorganisms that have been engineered to express one or more saccharifying enzymes.

Following hydrolyzation, a GVL-treated hydrolysate is contacted with one or more of the genetically engineered yeasts disclosed herein (e.g., a yeast strain genetically modified to exhibit reduced amounts of functional PAD1 polypeptide and/or functional FDC1 polypeptide) under conditions suitable for fermentation. Fermentation conditions can comprise aerobic or anaerobic conditions. In exemplary embodiments, a method of the invention comprises contacting under anaerobic conditions a recombinant yeast as provided herein to a GVL-treated hydrolysate for a period of time sufficient to allow fermentation of at least a portion of the cellulosic material into ethanol. In exemplary embodiments, a recombinant yeast used according to the methods provided herein is *Saccharomyces cerevisiae*. As used herein, "anaerobic fermentation" refers to a fermentation process run in the absence of oxygen or in which substantially no oxygen is consumed, preferably less than 5, 2.5, or 1 mmol/L/h, more preferably 0 mmol/L/h is consumed (i.e., oxygen consumption is not detectable), and where organic molecules serve as both electron donor and electron acceptors. In the absence of oxygen, NADH produced in glycolysis and biomass formation cannot be oxidized by oxidative phosphorylation.

In another aspect, the present invention provides a method of fermenting cellulosic material comprising the 5-carbon sugar xylose into ethanol, where the method comprises use of a recombinant yeast having enhanced tolerance of GVL relative to a wild type yeast or a recombinant yeast not comprising the genetic modifications described herein. In particular, the present invention provides a method whereby the rate of fermentation of cellulosic material in a GVL-treated hydrolysate to ethanol is increased relative to the fermentation rate of a GVL-treated hydrolysate not contacted to a recombinant yeast or yeast inoculum provided by the present invention. In such cases, the method comprises contacting a GVL-treated hydrolysate to a recombinant yeast having increased tolerance to GVL toxicity, whereby cellulosic material of the contacted hydrolysate is fermented to produce ethanol at an enhanced rate relative to fermentation of a GVL-treated hydrolysate that has not been contacted to a recombinant yeast of the present invention.

In some cases, methods of the present invention further comprise an ethanol separation or extraction step. Following conversion of sugars into ethanol, the ethanol can be separated from a fermentation culture using, for example, a standard distillation method or by filtration using membranes or membrane systems known in the art. Methods of separating or extracting are not restricted to those disclosed herein.

Methods of the present invention can be conducted continuously, batch-wise, or some combination thereof.

In some cases, a genetically engineered yeast disclosed herein can be used to produce ethanol from glycerol. Glycerol is a by-product of biodiesel production, which, using a recombinant yeast of the present invention, could be further converted to ethanol. In some cases, a method of converting glycerol to ethanol can comprise contacting glycerol to one or more of the genetically engineered yeasts disclosed herein (e.g., a yeast strain genetically modified to exhibit reduced amounts of functional PAD1 polypeptide and/or functional FDC1 polypeptide) under appropriate fermentation conditions. For example, a method of converting glycerol into ethanol can comprise contacting under anaerobic conditions

a recombinant yeast as provided herein to glycerol for a period of time sufficient to allow fermentation of at least a portion of the glycerol into ethanol. In exemplary embodiments, a recombinant yeast used according to the methods provided herein is *Saccharomyces cerevisiae* (*S. cerevisiae*).⁵ In some cases, the glycerol is crude glycerol.

Following conversion of glycerol into ethanol, the ethanol can be separated from a fermentation culture using, for example, a standard distillation method or by filtration using membranes or membrane systems known in the art. Methods of separating or extracting are not restricted to those disclosed or exemplified herein.¹⁰

Articles of Manufacture

In a further aspect, the present invention provides an article of manufacture containing any one or more of the recombinant yeasts disclosed herein is provided. An article of manufacture can contain one of the microorganisms disclosed herein (e.g., one or more of the yeast strains), or an article of manufacture can contain two or more of the microorganisms disclosed herein. Articles of manufacture disclosed herein also can include, for example, components necessary for growth of the particular microorganism(s).¹⁵

While the present invention is susceptible to various modifications and alternative forms, specific embodiments thereof have been shown by way of example in the drawings and are herein described in detail. It should be understood, however, that the description herein of specific embodiments is not intended to limit the invention to the particular forms disclosed, but on the contrary, the intention is to cover all modifications, equivalents and alternatives falling within the spirit and scope of the invention as defined by the appended claims.²⁰

The present invention will be more fully understood upon consideration of the following non-limiting Examples. All papers and patents disclosed herein are hereby incorporated by reference as if set forth in their entirety.²⁵

EXAMPLES

Genetic Engineering and Directed Evolution of a *S. cerevisiae* Strain Tolerant to GVL Toxicity³⁰

Lignocellulosic biomass derived fuels and chemicals provide a suite sustainable bioproducts. Before biomass can be converted to fuel or compounds, it must be converted to fermentable sugars (pre-treatment and hydrolysis), and these sugars converted to fuels by microorganisms. Both pre-treatment and hydrolysis can imbue the resultant hydrolysates with toxicity arising from residual pre-treatment chemicals or biomass derived inhibitors [2, 3], which throttle fermentation rates at a substantial economic cost [4].³⁵

Fermentation inhibitors come in many forms, and the landscape of these inhibitors is constantly changing as new pre-treatment, hydrolysis, and feedstocks technologies are developed [2]. Enzymatic hydrolysis of biomass for fermentation releases small acids, phenolics, and furans that are a ubiquitous challenge to bioconversion [3, 5]. Chemical hydrolysis methods such as γ -valerolactone (GVL) and ionic liquids offer an enzyme free route to fermentable sugars, but come with their own challenges [6-8]. In addition to the small acid inhibitors, the chemicals used for hydrolysis can persist in residual amounts into the resultant hydrolysate, and these compounds are not biologically benign to fermentative microorganisms [7, 8]. Further, as these chemical catalyst are used in relatively large amounts during hydrolysis, they residual concentrations are often much higher than the small acid and phenolic inhibitors generated from the biomass.⁴⁰
⁴⁵
⁵⁰
⁵⁵
⁶⁰
⁶⁵

GVL is a promising, new chemical hydrolysis technology to breakdown the cellulose polysaccharides to fermentable sugar monomers [6]. The advantage of GVL is that it is a recoverable and renewable chemical. One challenge of this method is the toxicity of residual GVL to fermentative microbes. GVL is mildly toxic to yeast, but this toxicity can be magnified when in combination with other inhibitors and the ethanol produced. As such, engineering GVL tolerant microbes is a means of overcoming toxicity, minimizing the costs of reagent recovery, and improving biofuels produced via ionic liquid hydrolysis.

We have used chemical genomics to discover the genome-wide response to toxicity. Using this information we have identified specific genes that mediate toxicity, and have engineered these specific mutations into an industrially viable, xylose-fermenting strain of *Saccharomyces cerevisiae*. This approach offer a rapid method of tailoring existing strains to specific chemical stressors found in industrial bioconversion.

GVL is the Major Inhibitor Found in GVL Hydrolysates:

GVL produced hydrolysates (FIG. 1A) are still largely unstudied, as such, our first goal was to identify the major inhibitors of GVL hydrolysates. LC/MS of hydrolysates revealed that three inhibitory compounds were highly abundant in the GVL hydrolysates: GVL, levulinic acid, and hydroxymethylfurfural (HMF); other lignocellulosic derived inhibitors were present, but at orders of magnitude lower concentrations (Table 1). GVL hydrolysates have a high level of residual GVL (230 mM), and as such this is the most toxic major inhibitor in GVL hydrolysates, given its half maximal inhibitory concentration (IC₅₀) is 270 mM (FIG. 1B). Because of this, we focused on understanding GVL toxicity and developing GVL-tolerant yeast strains.²⁵

TABLE 1

Quantification of the 10 most abundant fermentation inhibitors found in GVL hydrolysates	
Inhibitor	mM
GVL	100-230
Acetate	30.27
Formate	25.12
Levulinic acid	17.13
HMF	10.80
Acetaldehyde	1.98
Furfural	1.33
2-ketoglutaric acid	0.15
Furoic Acid	0.13
Coumaric acid	0.11

Chemical Genomic Predicts GVL Targets Cellular Membranes and Membrane Bound Processes:

To understand the mode of action of GVL toxicity we conducted chemical genomic analysis (FIG. 2A). This is a reverse genetics method that uses collections of defined gene mutants, and uses the response of these mutants in the presence of a chemical stress to gain functional insight into the chemical's mode of action and cellular target. We first challenged the yeast deletion collection with media containing 230 mM GVL and used barcode sequencing to identify the fitness response of the individual deletion mutants.

Among the top 10 sensitive deletion mutants, we found significant enrichment for genes involved in late endosome to vacuole transport ($p < 0.01$, FIG. 2B), driven by deletion mutants of SEC28, VPS38, DID2. We validated mutants within this GO terms using single mutants culture, and found all had a lower IC₅₀ compared to the control strain (FIG.

2C). Deletion mutants of these 3 genes have increased sensitivity to ethanol, heat, and membrane disrupting agents such as miconazole and nigericin. When we correlated the chemical genomic profile of GVL with the yeast genetic interaction network [10], we found significant enrichment for genes involved in golgi-vesicle mediated transport among the top 10 correlations ($p=0.001$). RET2 was consistently predicted as the top correlation for the GVL chemical genomic profile. Ret2p is a subunit of the coatmer complex involved in retrograde transport between Golgi and ER is also involved in golgi transport of vesicles [11]. RET2 mutants similarity show increased sensitivity to heat and membrane disrupting agents. We correlated the chemical genomic profile to GVL to existing chemical genomic datasets, and found its profile was significantly similar to profiles of nigericin ($p<0.01$) and papuamide ($p<0.01$), membrane destabilizing compounds. Taken together, these data suggest GVL could exert toxicity by damaging membrane integrity.

GVL Damages Membranes and is Synergistic with Ethanol:

To confirm if GVL treatment can rapidly affect cell integrity, we assessed cell permeability after GVL treatment. Using FACS analysis combined with a dye that is only taken up by cells with damaged membranes, we found a rapid and dose dependent effect of GVL on leakage (FIGS. 3A, 3B), similar to the effects of ethanol but with a greater magnitude (FIG. 3B). Given that both GVL and ethanol can damage cellular membranes, we also tested if these compounds are synergistic. We found a strong synergism between GVL and ethanol in both our lab strain and xylose fermenting strain (FIG. 3C). At a 1% GVL concentration and 4% ethanol concentration, we saw a significant synergistic interaction between GVL and ethanol ($p<0.01$). This suggest that as ethanol titers increase during fermentation, the toxic effects of GVL and ethanol will magnify each other, which ultimately affects yield.

Deletion of the Decarboxylases Pad1p and Fdc1p Enhance GVL Tolerance:

Importantly for our goal, we also looked for gene deletions that increased resistance to GVL. Among the top GVL resistance mutants we found a significant enrichment for genes involved in phenylpropanoid metabolic process ($p<0.002$, FIG. 4A), driven by deletion mutants of PAD1 and FDC1. Single mutant validations reveals deletion of these genes improved GVL tolerance (FIG. 4B). Pad1p is phenylacrylic acid decarboxylase with a reported role in aromatic acid catabolism and the ability to detoxify cinnamic acid [12, 13]. Like Pad1p, Fdc1p is thought to be a similar phenylacrylic acid decarboxylase involved in detoxifying ferulic acid [13].

Using chemical genomics guided biodesign, we identified 2 genes that are key in mediating GVL tolerance of the fermentative yeast *S. cerevisiae*. Deletion of the genes encoding acid decarboxylases Pad1 and Fdc1 conferred greater tolerance to GVL. These specific mutations were introduced into to an industrially viable, xylose fermenting yeast (GLBRCY-128) to create a ethanol producing yeast (GVL-R1) specifically tailored for GVL hydrolysates. Yeast of the GVL-R1 strain has the advantage of being able to grow and ferment both glucose and xylose faster than the GLBRC-Y128 strain in up to 2.5% residual GVL. Under our test conditions, GLBRC-Y128 required 72 hours to completely ferment all glucose, whereas engineered strain GVL-R1 achieved this in 48 hours. Importantly, engineered strain GVL-R1 was also able to ferment xylose, allowing for greater ethanol yields.

Overexpression Chemical Genomic Profiling Confirms Pad1p Mediates GVL Toxicity:

We wanted to extend our chemical genomic analysis to industrially an industrially relevant, xylose fermenting yeast strain. Presently there are no available genome-wide deletion mutant collections in industrial yeast, so we took a complementary approach. The MoBY-ORF 2.0 plasmid collection is with barcoded versions of 95% of all *S. cerevisiae* genes each expressed on a 2 μ plasmid [14]. This collection of plasmids can be pooled and transformed into any yeast to allow investigations of the effect of gene dose under stress conditions. We transformed a version of the xylose-fermenting yeast GLBRC-Y133 [15] en masse with the pooled plasmid collection and selected over 50K individual transformants (10 \times genome coverage). We grew this pooled transformant collection in the presence of 2.5% GVL or a water control under anaerobic conditions in glucose/xylose containing media and assessed the effects of increased gene dose on growth in the presence of GVL. We found the Pad1p overexpression mutant was one of the top sensitive strains ($p<0.01$, FIG. 4C). We confirmed with single mutant cultures that overexpression of PAD1 causes GVL sensitivity. The IC_{50} of Y133+ pPAD1 was 2.2%, compared to 2.56% of vector control (FIG. 4D, $p<0.001$).

Deletion of PAD1 and FDC1 in a Xylose Fermenting Strain Confers GVL Tolerance:

Chemical genomic profiling and validation of individual mutants confirmed that the decarboxylase Pad1p (and Fdc1p) were involved in GVL toxicity. We chose to engineer these deletions into a xylose fermenting yeast strain GLBRC Y133 (henceforth Y133). PAD1 and FDC1 are adjacent on chromosome IV, and as such we were able to delete both at the same time using transformation with PCR product of the antibiotic resistance marker KanMX flanked by homologous regions upstream of PAM and downstream of FDC1 (FIG. 4A). We confirmed deletion of both genes by PCR (FIG. 4B).

The IC_{50} concentration of GVL of the Y133 pad1 Δ fdc1 Δ strain was significantly higher than the Y133 background (FIG. 5C; $p<0.01$). Finally, we tested the performance of the Y133 pad1 Δ fdc1 Δ strain under industrially relevant anaerobic conditions in a synthetic hydrolysate containing 1% GVL. The double KO strain grew, consumed sugars, and produced ethanol, whereas the Y133 background strain did not (FIG. 5D).

Vinyl Products of Pad1p Decarboxylation are Synergistic with GVL:

PAD1 and FDC1 are known to convert phenolic acids into a vinyl form, and are thought to “detoxify” ferulic and coumaric acids; however, we posit that the vinyl derivatives (see FIG. 6A) may be more toxic than the acid forms. We found that the IC_{50} values of the vinyl derivative of coumaric acid, 4-vinylphenol, was an order of magnitude lower than that of coumaric acid (FIG. 6B). Further, we found a statistically significant synergistic interaction between the vinyl derivative of coumaric acid, 4-vinylphenol, and GVL (FIG. 6C, $p<0.01$). Chemical genomic profiling of 4-vinylphenol revealed that, similar to GVL, RET2 was the top genetic interaction network correlation, and this compound was similarly predicted to target the membrane bound processes such as vesicle mediated transport. Deletion of PAD1 and FDC1 may reduce production of membrane damaging vinyls, which are synergistic with GVL. Our Y133 pad1 Δ fdc1 Δ has a statistically significantly greater tolerance of coumaric acid (FIG. 6D, $p<0.01$), and we contend this is because less of the more toxic vinyl form is being generated.

Discussion

Through chemical genomic analysis we predicted and confirmed the chemical hydrolysis reagent gamma-valerolactone exerts toxicity by damaging cellular membranes, similar to ethanol and other membrane damaging drugs. Further, this compound is synergistic with ethanol. While this compound is less toxic than other fermentation inhibitors (e.g., furfural, HMF), the abundance of residual GVL in hydrolysates may ultimately limit ethanol production through a documented synergism with end-product fuels such as ethanol or isobutanol. The toxic effects of GVL can be alleviated by specific deletion of the cellular decarboxylases Pad1p and Fdc1p, which convert phenolic acids into a more toxic vinyl form that is synergistic with GVL. While these specific decarboxylases have been studied for their role in 'detoxifying' hydrolysates by converting phenolic acids, the vinyl products may ultimately have a greater effect on growth in phenolic rich hydrolysates.

The process technologies of lignocellulosic biofuel production are still evolving, and as a result the landscape of fermentation inhibitors is dynamic. Strain development is necessary to keep pace with these new chemical stressors. Industry relies on tried and true industrial yeast strains with favorable performance and may be hesitant to adopt new genetic backgrounds, no matter how well they are predicted to perform. We have used a functional genomics approach to identify points of rational engineering. As our discovery system is based on *Saccharomyces cerevisiae*, the primary bioethanol organism, these genes identified can be directly modified in other yeast strains to rapidly tailor proven strains to new purposes.

This approach can also be applied to other bioproducts. Through synthetic biology drugs, green chemicals, and next-generation fuels can be produced by yeast and other engineered microbes, and many of these end-products can be toxic to the producing biocatalyst. The genome-wide, functional view of their effects provided by chemical genomics could be useful in improving production. This system is not limited to yeast, genomic wide mutant and overexpression collections exist in a number of industrial relevant microbes, such as *E. coli* and *Zymomonas mobilis*, and as such, the same approach is translatable.

Methods

Compounds, Initial Screening, and IC₅₀ Determination:

Compounds tested were purchased from Sigma. Cells of *S. cerevisiae* (MAT α pdr1 Δ ::natMX pdr3 Δ ::KI.URA3 snq2 Δ ::K1.LEU2 can1 Δ ::STE2pr-Sp_his5 lyp1 Δ his3 Δ 1 leu2 Δ 0 ura3 Δ 0 met15 Δ 0), referred to as control strain, were grown in 200 μ l cultures at 30° C. in YPD, with a drug or DMSO control. Plates were read on a TECAN M1000 over a 48 h growth period. The specific growth rate was calculated using GCAT analysis software (available at gcat3-pub.glbrc.org on the world wide web) [16]. When presented, IC₅₀ values for growth inhibition were calculated from triplicate 8 point dose curves and SigmaPlot 12.0. When presented, error bars are Mean \pm Standard error of at least 3 replicates.

Chemical Genomic Analysis:

Chemical genomic analysis of poaic acid was performed as described as described previously [17, 18]. The tested yeast deletion collection had ~4000 strains using the genetic background described in Andrusiak (2012) [19]. The optimal inhibitory concentration of poaic acid for chemical genomic profiling (70-80% growth versus solvent control in YP-galactose media after 24 hours of growth) was determined using an 8 point dose curve. A concentration of 88 μ g/ml inhibited growth within this range. 200 μ l cultures of the pooled, deletion collection of *S. cerevisiae* deletion mutants were grown with 88 μ g/ml poaic acid or a DMSO control in triplicate for 48 h at 30° C. Genomic DNA was

extracted using the Epicentre MasterPure™ Yeast DNA purification kit. Mutant-specific molecular barcodes were amplified with specially designed multiplex primers [20]. The barcodes were sequenced using an Illumina MiSeq. 3 replicates of each condition (poaic acid vs DMSO) were sequenced. One DMSO control was lost due to poor sequencing reads. The barcode counts for each yeast deletion mutant in the presence of poaic acid were normalized against the DMSO control conditions to define sensitivity or resistance of individual strains. To determine a p-value for each top sensitive and resistant mutant, we used the EdgeR package [21, 22]. A Bonferroni-corrected hypergeometric distribution test was used to search for significant enrichment of GO terms among the top 10 sensitive and resistant deletion mutants [23]. To understand the pathways that were most affected by poaic acid we developed a protein complex/pathway score based on the summation of the z-scores for each complex/pathway (Pathway z-score). Correlation of the chemical genomic profile of poaic acid with the yeast genetic interaction network to was done as described in Costanzo et al. (2010) [10].

MoBY-ORF Profiling:

MoBY-ORF profiling of GVL was conducted by first generating a pooled collection of the yeast GLBRC-Y133 containing the plasmid collection. The plasmid pool for transformation was generated as described previously (HO). For yeast transformation, the plasmids were extracted from 150 mL of *E. coli* culture MAXI Prep. Plasmid was used to transform GLBRC-Y133 via high efficiency LiAc transformation. Transformed yeast were plated to YPD+Geneticin (G418) agar plates and incubated until colonies appeared. A total of 50,000 colonies were washed from the plates using 1 \times PBS, mixed 1:1 with 50% glycerol, and stored until use. For MoBY-ORF profiling, 25 mL of media containing YPD+2.5% GVL+G418 was allowed to degas overnight in an anaerobic chamber, and then inoculated with 100 μ l of the transformed yeast pool (n=3). Cells were grown in culture for 48 hours. Genomic DNA was extracted from 1 mL from each culture using modified mini-prep with with zymolyase and glass beads. Gene specific barcodes were amplified, processed, sequenced, and analyzed as described above.

Growth and Sugar Conversion Experiments:

6 25-mL anaerobic flasks were prepared with Synthetic hydrolysate (SynH) (6% glucose/3% xylose)+1% GVL, pH 5.0. Flasks were inoculated with rinsed 133 or 133 pad1 Δ fdc1 Δ cells to bring the initial OD to approximately 0.1. The tubes were grown for 72 hours with agitation anaerobically at 30° C. 1 mL samples were taken every 24 hours. Initial and daily samples were measured for OD and submitted for HPLC analysis to quantify sugar consumption and ethanol production.

Cell Leakage Assays:

A FungaLight™ cell viability assay (Invitrogen L34952) was used to determine if poaic acid caused membrane damage we used using a Guava Flow Cytometer (Millipore, USA). The population of stained cells (damaged integrity) vs non-stained cells can be determined by flow cytometry. Caspofungin (50 ng/ml) was included as a positive control. MMS and DMSO were included as a non-cell wall targeting and solvent control respectively. To test the effects of the compounds on both active and arrested cells, log-phase cultures were washed with 1 \times PBS and resuspended to an OD of 0.5 in either YPD media or YP (no carbon source) in the presence of the drugs (n=3) for 4 hours at 30° C. The cells were then stained and immediately read by flow cytometry. A one-way ANOVA and Tukey's test was used to calculate the difference between drug treatments among cells with arrested growth.

Synergy Screening:

To test for synergy, a 6×6 dose matrix was initially used to identify potentially synergistic dose combinations, these points were then confirmed in triplicate. 200 µl cultures were grown with combinations of with poacic acid (125 µg/ml), caspofungin (12.5 ng/ml) and fluconazole (3.8 µg/ml) and the relevant single agent and solvent controls their OD measured after 24 h. Synergy was determined by comparing actual optical density in the presence of compound combinations to an expected value calculated using the multiplicative hypothesis. This assumes that, in the absence of an interaction, each compound would decrease the OD of the cell culture by the same fraction in the presence of the other compound as it does when applied alone, i.e., $E=A*B/C$, where E is the expected OD, A is OD when compound A is applied alone, B is OD when compound B is applied alone, and C is OD of the control culture (DMSO). In the presence of synergy, the actual OD value is lower than the expected OD. A paired t-test was used to confirm statistical significance of this difference in 3 replicates of the experiment.

Determination of Ferulate and Diferulates by RP-HPLC-HR/AM-MS in Hydrolysates:

ACSH samples were diluted 1:10 and 20 µL samples were analyzed by reverse phase (C18) HPLC—high resolution/accurate mass spectrometry. Peak areas of peaks matching in retention time and accurate mass±10 ppm of authentic reference standards were used to calculate concentrations by comparison to an external standard curve.

GVL Synergy Experiments:

The synergistic interaction between GVL and ethanol was initially discovered using a 6-point dose matrix of the two compounds. We identified the points of the greatest synergy and perform triplicate growth curves of GLBRY-128 using a TECAN M1000 microplate reader. To confirm the GVL-R1 strain was less sensitive to the synergism between GVL and ethanol, used a 6-point dose matrix as described above with both GLBRCY-128 or GVL-R1 in a TECAN microplate reader for 48 hours at 30° C. Data from the most synergistic combination is presented (2% GVL-5% ethanol).

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<211> LENGTH: 3079

<212> TYPE: PRT

<213> ORGANISM: *Saccharomyces cerevisiae*

<400> SEQUENCE: 2

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20          25          30
Arg Ile Leu Pro Ile Leu Pro Val Glu Ser Asn Leu Ser Thr Tyr Ser
35          40          45
Glu Val Glu Glu Tyr Ser Ser Phe Ile Ser Cys Arg Ser Val Leu Ile
50          55          60
Asn Val Thr Val Ser Arg Asp Ala Asn Ala Met Val Glu Gly Thr Leu
65          70          75          80
Glu Leu Ile Glu Ser Leu Leu Gln Gly His Glu Ile Ile Ser Asp Lys
85          90          95
Gly Ser Ser Asp Val Ile Glu Ser Ile Leu Ile Ile Leu Arg Leu Leu
100         105         110
Ser Asp Ala Leu Glu Tyr Asn Trp Gln Asn Gln Glu Ser Leu His Tyr
115         120         125
Asn Asp Ile Ser Thr His Val Glu His Asp Gln Glu Gln Lys Tyr Arg
130         135         140
Pro Lys Leu Asn Ser Ile Leu Pro Asp Tyr Ser Ser Thr His Ser Asn
145         150         155         160
Gly Asn Lys His Phe Phe His Gln Ser Lys Pro Gln Ala Leu Ile Pro
165         170         175
Glu Leu Ala Ser Lys Leu Leu Glu Ser Cys Ala Lys Leu Lys Phe Asn
180         185         190
Thr Arg Thr Leu Gln Ile Leu Gln Asn Met Ile Ser His Val His Gly
195         200         205
Asn Ile Leu Thr Thr Leu Ser Ser Ser Ile Leu Pro Arg His Lys Ser
210         215         220
Tyr Leu Thr Arg His Asn His Pro Ser His Cys Lys Met Ile Asp Ser
225         230         235         240
Thr Leu Gly His Ile Leu Arg Phe Val Ala Ala Ser Asn Pro Ser Glu
245         250         255
Tyr Phe Glu Phe Ile Arg Lys Ser Val Gln Val Pro Val Thr Gln Thr
260         265         270
His Thr His Ser His Ser His Ser His Ser Leu Pro Ser Ser Val Tyr
275         280         285
Asn Ser Ile Val Pro His Phe Asp Leu Phe Ser Phe Ile Tyr Leu Ser
290         295         300
Lys His Asn Phe Lys Lys Tyr Leu Glu Leu Ile Lys Asn Leu Ser Val
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Thr Leu Arg Lys Thr Ile Tyr His Cys Leu Leu Leu His Tyr Ser Ala
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Lys Ala Ile Met Phe Trp Ile Met Ala Arg Pro Ala Glu Tyr Tyr Glu
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Leu Phe Asn Leu Leu Lys Asp Asn Asn Asn Glu His Ser Lys Ser Leu
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Asn Thr Leu Asn His Thr Leu Phe Glu Glu Ile His Ser Thr Phe Asn
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Val Asn Ser Met Ile Thr Thr Asn Gln Asn Ala His Gln Gly Ser Ser
 385 390 395 400

Ser Pro Ser Ser Ser Ser Pro Ser Ser Pro Pro Ser Ser Ser Ser Ser
 405 410 415

Asp Asn Asn Asn Gln Asn Ile Ile Ala Lys Ser Leu Ser Arg Gln Leu
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Ser His His Gln Ser Tyr Ile Gln Gln Gln Ser Glu Arg Lys Leu His
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Ser Ser Trp Thr Thr Asn Ser Gln Ser Ser Thr Ser Leu Ser Ser Ser
 450 455 460

Thr Ser Asn Ser Thr Thr Thr Asp Phe Ser Thr His Thr Gln Pro Gly
 465 470 475 480

Glu Tyr Asp Pro Ser Leu Pro Asp Thr Pro Thr Met Ser Asn Ile Thr
 485 490 495

Ile Ser Ala Ser Ser Leu Leu Ser Gln Thr Pro Thr Pro Thr Thr Gln
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Leu Gln Gln Arg Leu Asn Ser Ala Ala Ala Ala Ala Ala Ala Ala Ala
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Ser Pro Ser Asn Ser Thr Pro Thr Gly Tyr Thr Ala Glu Gln Gln Ser
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Arg Ala Ser Tyr Asp Ala His Lys Thr Gly His Thr Gly Lys Asp Tyr
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Asp Glu His Phe Leu Ser Val Thr Arg Leu Asp Asn Val Leu Glu Leu
 565 570 575

Tyr Thr His Phe Asp Asp Thr Glu Val Leu Pro His Thr Ser Val Leu
 580 585 590

Lys Phe Leu Thr Thr Leu Thr Met Phe Asp Ile Asp Leu Phe Asn Glu
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Leu Asn Ala Thr Ser Phe Lys Tyr Ile Pro Asp Cys Thr Met His Arg
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Pro Lys Glu Arg Thr Ser Ser Phe Asn Asn Thr Ala His Glu Thr Gly
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Ser Glu Lys Thr Ser Gly Ile Lys His Ile Thr Gln Gly Leu Lys Lys
 645 650 655

Leu Thr Ser Leu Pro Ser Ser Thr Lys Lys Thr Val Lys Phe Val Lys
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Met Leu Leu Arg Asn Leu Asn Gly Asn Gln Ala Val Ser Asp Val Ala
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Leu Leu Asp Thr Met Arg Ala Leu Leu Ser Phe Phe Thr Met Thr Ser
 690 695 700

Ala Val Phe Leu Val Asp Arg Asn Leu Pro Ser Val Leu Phe Ala Lys
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Arg Leu Ile Pro Ile Met Gly Thr Asn Leu Ser Val Gly Gln Asp Trp
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Asn Ser Lys Ile Asn Asn Ser Leu Met Val Cys Leu Lys Lys Asn Ser
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 Ile Phe Phe Asp Ile Pro Ser Lys Lys Glu Leu Arg Lys Ala Ile Ala
 805 810 815
 Val Lys Ile Ser Lys Phe Phe Lys Thr Leu Phe Ser Ile Ile Ala Asp
 820 825 830
 Ile Leu Leu Gln Glu Phe Pro Tyr Phe Asp Glu Gln Ile Thr Asp Ile
 835 840 845
 Val Ala Ser Ile Leu Asp Gly Thr Ile Ile Asn Glu Tyr Gly Thr Lys
 850 855 860
 Lys His Phe Lys Gly Ser Ser Pro Ser Leu Cys Ser Thr Thr Arg Ser
 865 870 875 880
 Arg Ser Gly Ser Thr Ser Gln Ser Ser Met Thr Pro Val Ser Pro Leu
 885 890 895
 Gly Leu Asp Thr Asp Ile Cys Pro Met Asn Thr Leu Ser Leu Val Gly
 900 905 910
 Ser Ser Thr Ser Arg Asn Ser Asp Asn Val Asn Ser Leu Asn Ser Ser
 915 920 925
 Pro Lys Asn Leu Ser Ser Asp Pro Tyr Leu Ser His Leu Val Ala Pro
 930 935 940
 Arg Ala Arg His Ala Leu Gly Gly Pro Ser Ser Ile Ile Arg Asn Lys
 945 950 955 960
 Ile Pro Thr Thr Leu Thr Ser Pro Pro Gly Thr Glu Lys Ser Ser Pro
 965 970 975
 Val Gln Arg Pro Gln Thr Glu Ser Ile Ser Ala Thr Pro Met Ala Ile
 980 985 990
 Thr Asn Ser Thr Pro Leu Ser Ser Ala Ala Phe Gly Ile Arg Ser Pro
 995 1000 1005
 Leu Gln Lys Ile Arg Thr Arg Arg Tyr Ser Asp Glu Ser Leu Gly
 1010 1015 1020
 Lys Phe Met Lys Ser Thr Asn Asn Tyr Ile Gln Glu His Leu Ile
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 Pro Lys Asp Leu Asn Glu Ala Thr Leu Gln Asp Ala Arg Arg Ile
 1040 1045 1050
 Met Ile Asn Ile Phe Ser Ile Phe Lys Arg Pro Asn Ser Tyr Phe
 1055 1060 1065
 Ile Ile Pro His Asn Ile Asn Ser Asn Leu Gln Trp Val Ser Gln
 1070 1075 1080
 Asp Phe Arg Asn Ile Met Lys Pro Ile Phe Val Ala Ile Val Ser
 1085 1090 1095
 Pro Asp Val Asp Leu Gln Asn Thr Ala Gln Ser Phe Met Asp Thr
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 Leu Leu Ser Asn Val Ile Thr Tyr Gly Glu Ser Asp Glu Asn Ile
 1115 1120 1125
 Ser Ile Glu Gly Tyr His Leu Leu Cys Ser Tyr Thr Val Thr Leu
 1130 1135 1140
 Phe Ala Met Gly Leu Phe Asp Leu Lys Ile Asn Asn Glu Lys Arg
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Gln Ile	Leu Leu Asp	Ile Thr	Val Lys Phe Met	Lys	Val Arg Ser
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Ser Asp	Ser Glu Lys Leu	Thr	Phe Pro Leu Ile	Met	Gly Thr Val
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Gly Arg	Ala Leu Phe Val	Ser	Leu Tyr Ser Ser	Gln	Gln Lys Ile
1205		1210		1215	
Glu Lys	Thr Leu Lys Ile	Ala	Tyr Thr Glu Tyr	Leu	Ser Ala Ile
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Asn Phe	His Glu Arg Asn	Ile	Asp Asp Ala Asp	Lys	Thr Trp Val
1235		1240		1245	
His Asn	Ile Glu Phe Val	Glu	Ala Met Cys His	Asp	Asn Tyr Thr
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Thr Ser	Gly Ser Ile Ala	Phe	Gln Arg Arg Thr	Arg	Asn Asn Ile
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Leu Arg	Phe Ala Thr Ile	Pro	Asn Ala Ile Leu	Leu	Asp Ser Met
1280		1285		1290	
Arg Met	Ile Tyr Lys Lys	Trp	His Thr Tyr Thr	His	Ser Lys Ser
1295		1300		1305	
Leu Glu	Lys Gln Glu Arg	Asn	Asp Phe Arg Asn	Phe	Ala Gly Ile
1310		1315		1320	
Leu Ala	Ser Leu Ser Gly	Ile	Leu Phe Ile Asn	Lys	Lys Ile Leu
1325		1330		1335	
Gln Glu	Met Tyr Pro Tyr	Leu	Leu Asp Thr Val	Ser	Glu Leu Lys
1340		1345		1350	
Lys Asn	Ile Asp Ser Phe	Ile	Ser Lys Gln Cys	Gln	Trp Leu Asn
1355		1360		1365	
Tyr Pro	Asp Leu Leu Thr	Arg	Glu Asn Ser Arg	Asp	Ile Leu Ser
1370		1375		1380	
Val Glu	Leu His Pro Leu	Ser	Phe Asn Leu Leu	Phe	Asn Asn Leu
1385		1390		1395	
Arg Leu	Lys Leu Lys Glu	Leu	Ala Cys Ser Asp	Leu	Ser Ile Pro
1400		1405		1410	
Glu Asn	Glu Ser Ser Tyr	Val	Leu Leu Glu Gln	Ile	Ile Lys Met
1415		1420		1425	
Leu Arg	Thr Ile Leu Gly	Arg	Asp Asp Asp Asn	Tyr	Val Met Met
1430		1435		1440	
Leu Phe	Ser Thr Glu Ile	Val	Asp Leu Ile Asp	Leu	Leu Thr Asp
1445		1450		1455	
Glu Ile	Lys Lys Ile Pro	Ala	Tyr Cys Pro Lys	Tyr	Leu Lys Ala
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Ile Ile	Gln Met Thr Lys	Met	Phe Ser Ala Leu	Gln	His Ser Glu
1475		1480		1485	
Val Asn	Leu Gly Val Lys	Asn	His Phe His Val	Lys	Asn Lys Trp
1490		1495		1500	
Leu Arg	Gln Ile Thr Asp	Trp	Phe Gln Val Ser	Ile	Ala Arg Glu
1505		1510		1515	
Tyr Asp	Phe Glu Asn Leu	Ser	Lys Pro Leu Lys	Glu	Met Asp Leu
1520		1525		1530	
Val Lys	Arg Asp Met Asp	Ile	Leu Tyr Ile Asp	Thr	Ala Ile Glu
1535		1540		1545	

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Ala Ser 1550	Thr Ala Ile Ala Tyr 1555	Leu Thr Arg His 1560	Thr Phe Leu Glu
Ile Pro 1565	Pro Ala Ala Ser Asp 1570	Pro Glu Leu Ser 1575	Arg Ser Arg Ser
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Lys Ser 1595	Ser Asp Arg Asp Asn 1600	Tyr Pro Val Phe 1605	Leu Arg His Lys
Met Ser 1610	Val Leu Asn Asp Asn 1615	Val Ile Leu Ser 1620	Leu Thr Asn Leu
Ser Asn 1625	Thr Asn Val Asp Ala 1630	Ser Leu Gln Phe 1635	Thr Leu Pro Met
Gly Tyr 1640	Ser Gly Asn Arg Asn 1645	Ile Arg Asn Ala 1650	Phe Leu Glu Val
Phe Ile 1655	Asn Ile Val Thr Asn 1660	Tyr Arg Thr Tyr 1665	Thr Ala Lys Thr
Asp Leu 1670	Gly Lys Leu Glu Ala 1675	Ala Asp Lys Phe 1680	Leu Arg Tyr Thr
Ile Glu 1685	His Pro Gln Leu Ser 1690	Ser Phe Gly Ala 1695	Ala Val Cys Pro
Ala Ser 1700	Asp Ile Asp Ala Tyr 1705	Ala Ala Gly Leu 1710	Ile Asn Ala Phe
Glu Thr 1715	Arg Asn Ala Thr His 1720	Ile Val Val Ala 1725	Gln Leu Ile Lys
Asn Glu 1730	Ile Glu Lys Ser Ser 1735	Arg Pro Thr Asp 1740	Ile Leu Arg Arg
Asn Ser 1745	Cys Ala Thr Arg Ser 1750	Leu Ser Met Leu 1755	Ala Arg Ser Lys
Gly Asn 1760	Glu Tyr Leu Ile Arg 1765	Thr Leu Gln Pro 1770	Leu Leu Lys Lys
Ile Ile 1775	Gln Asn Arg Asp Phe 1780	Phe Glu Ile Glu 1785	Lys Leu Lys Pro
Glu Asp 1790	Ser Asp Ala Glu Arg 1795	Gln Ile Glu Leu 1800	Phe Val Lys Tyr
Met Asn 1805	Glu Leu Leu Glu Ser 1810	Ile Ser Asn Ser 1815	Val Ser Tyr Phe
Pro Pro 1820	Pro Leu Phe Tyr Ile 1825	Cys Gln Asn Ile 1830	Tyr Lys Val Ala
Cys Glu 1835	Lys Phe Pro Asp His 1840	Ala Ile Ile Ala 1845	Ala Gly Ser Phe
Val Phe 1850	Leu Arg Phe Phe Cys 1855	Pro Ala Leu Val 1860	Ser Pro Asp Ser
Glu Asn 1865	Ile Ile Asp Ile Ser 1870	His Leu Ser Glu 1875	Lys Arg Thr Phe
Ile Ser 1880	Leu Ala Lys Val Ile 1885	Gln Asn Ile Ala 1890	Asn Gly Ser Glu
Asn Phe 1895	Ser Arg Trp Pro Ala 1900	Leu Cys Ser Gln 1905	Lys Asp Phe Leu
Lys Glu 1910	Cys Ser Asp Arg Ile 1915	Phe Arg Phe Leu 1920	Ala Glu Leu Cys
Arg Thr 1925	Asp Arg Thr Ile Asp 1930	Ile Gln Val Arg 1935	Thr Asp Pro Thr

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Pro 1940	Ile	Ala	Phe	Asp	Tyr	Gln	Phe	Leu	His	Ser	Phe	Val	Tyr	Leu
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Tyr 1955	Gly	Leu	Glu	Val	Arg	Arg	Asn	Val	Leu	Asn	Glu	Ala	Lys	His
						1960					1965			
Asp 1970	Asp	Gly	Asp	Ile	Asp	Gly	Asp	Asp	Phe	Tyr	Lys	Thr	Thr	Phe
						1975					1980			
Leu 1985	Leu	Ile	Asp	Asp	Val	Leu	Gly	Gln	Leu	Gly	Gln	Pro	Lys	Met
						1990					1995			
Glu 2000	Phe	Ser	Asn	Glu	Ile	Pro	Ile	Tyr	Ile	Arg	Glu	His	Met	Asp
						2005					2010			
Asp 2015	Tyr	Pro	Glu	Leu	Tyr	Glu	Phe	Met	Asn	Arg	His	Ala	Phe	Arg
						2020					2025			
Asn 2030	Ile	Glu	Thr	Ser	Thr	Ala	Tyr	Ser	Pro	Ser	Val	His	Glu	Ser
						2035					2040			
Thr 2045	Ser	Ser	Glu	Gly	Ile	Pro	Ile	Ile	Thr	Leu	Thr	Met	Ser	Asn
						2050					2055			
Phe 2060	Ser	Asp	Arg	His	Val	Asp	Ile	Asp	Thr	Val	Ala	Tyr	Lys	Phe
						2065					2070			
Leu 2075	Gln	Ile	Tyr	Ala	Arg	Ile	Trp	Thr	Thr	Lys	His	Cys	Leu	Ile
						2080					2085			
Ile 2090	Asp	Cys	Thr	Glu	Phe	Asp	Glu	Gly	Gly	Leu	Asp	Met	Arg	Lys
						2095					2100			
Phe 2105	Ile	Ser	Leu	Val	Met	Gly	Leu	Leu	Pro	Glu	Val	Ala	Pro	Lys
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Asn 2120	Cys	Ile	Gly	Cys	Tyr	Tyr	Phe	Asn	Val	Asn	Glu	Thr	Phe	Met
						2125					2130			
Asp 2135	Asn	Tyr	Gly	Lys	Cys	Leu	Asp	Lys	Asp	Asn	Val	Tyr	Val	Ser
						2140					2145			
Ser 2150	Lys	Ile	Pro	His	Tyr	Phe	Ile	Asn	Ser	Asn	Ser	Asp	Glu	Gly
						2155					2160			
Leu 2165	Met	Lys	Ser	Val	Gly	Ile	Thr	Gly	Gln	Gly	Leu	Lys	Val	Leu
						2170					2175			
Gln 2180	Asp	Ile	Arg	Val	Ser	Leu	His	Asp	Ile	Thr	Leu	Tyr	Asp	Glu
						2185					2190			
Lys 2195	Arg	Asn	Arg	Phe	Thr	Pro	Val	Ser	Leu	Lys	Ile	Gly	Asp	Ile
						2200					2205			
Tyr 2210	Phe	Gln	Val	Leu	His	Glu	Thr	Pro	Arg	Gln	Tyr	Lys	Ile	Arg
						2215					2220			
Asp 2225	Met	Gly	Thr	Leu	Phe	Asp	Val	Lys	Phe	Asn	Asp	Val	Tyr	Glu
						2230					2235			
Ile 2240	Ser	Arg	Ile	Phe	Glu	Val	His	Val	Ser	Ser	Ile	Thr	Gly	Val
						2245					2250			
Ala 2255	Ala	Glu	Phe	Thr	Val	Thr	Phe	Gln	Asp	Glu	Arg	Arg	Leu	Ile
						2260					2265			
Phe 2270	Ser	Ser	Pro	Lys	Tyr	Leu	Glu	Ile	Val	Lys	Met	Phe	Tyr	Tyr
						2275					2280			
Ala 2285	Gln	Ile	Arg	Leu	Glu	Ser	Glu	Tyr	Glu	Met	Asp	Asn	Asn	Ser
						2290					2295			
Ser 2300	Thr	Ser	Ser	Pro	Asn	Ser	Asn	Asn	Lys	Asp	Lys	Gln	Gln	Lys
						2305					2310			
Glu 2315	Arg	Thr	Lys	Leu	Leu	Cys	His	Leu	Leu	Leu	Val	Ser	Leu	Ile
						2320					2325			

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Gly	Leu	Phe	Asp	Glu	Ser	Lys	Lys	Met	Lys	Asn	Ser	Ser	Tyr	Asn
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2345						2350					2355			
His	Phe	His	Arg	Ser	Pro	Glu	Val	Tyr	Val	Pro	Glu	Asp	Thr	Thr
2360						2365					2370			
Thr	Phe	Leu	Gly	Val	Ile	Gly	Lys	Ser	Leu	Ala	Glu	Ser	Asn	Pro
2375						2380					2385			
Glu	Leu	Thr	Ala	Tyr	Met	Phe	Ile	Tyr	Val	Leu	Glu	Ala	Leu	Lys
2390						2395					2400			
Asn	Asn	Val	Ile	Pro	His	Val	Tyr	Ile	Pro	His	Thr	Ile	Cys	Gly
2405						2410					2415			
Leu	Ser	Tyr	Trp	Ile	Pro	Asn	Leu	Tyr	Gln	His	Val	Tyr	Leu	Ala
2420						2425					2430			
Asp	Asp	Glu	Glu	Gly	Pro	Glu	Asn	Ile	Ser	His	Ile	Phe	Arg	Ile
2435						2440					2445			
Leu	Ile	Arg	Leu	Ser	Val	Arg	Glu	Thr	Asp	Phe	Lys	Ala	Val	Tyr
2450						2455					2460			
Met	Gln	Tyr	Val	Trp	Leu	Leu	Leu	Leu	Asp	Asp	Gly	Arg	Leu	Thr
2465						2470					2475			
Asp	Ile	Ile	Val	Asp	Glu	Val	Ile	Asn	His	Ala	Leu	Glu	Arg	Asp
2480						2485					2490			
Ser	Glu	Asn	Arg	Asp	Trp	Lys	Lys	Thr	Ile	Ser	Leu	Leu	Thr	Val
2495						2500					2505			
Leu	Pro	Thr	Thr	Glu	Val	Ala	Asn	Asn	Ile	Ile	Gln	Lys	Ile	Leu
2510						2515					2520			
Ala	Lys	Ile	Arg	Ser	Phe	Leu	Pro	Ser	Leu	Lys	Leu	Glu	Ala	Met
2525						2530					2535			
Thr	Gln	Ser	Trp	Ser	Glu	Leu	Thr	Ile	Leu	Val	Lys	Ile	Ser	Ile
2540						2545					2550			
His	Val	Phe	Phe	Glu	Thr	Ser	Leu	Leu	Val	Gln	Met	Tyr	Leu	Pro
2555						2560					2565			
Glu	Ile	Leu	Phe	Ile	Val	Ser	Leu	Leu	Ile	Asp	Val	Gly	Pro	Arg
2570						2575					2580			
Glu	Leu	Arg	Ser	Ser	Leu	His	Gln	Leu	Leu	Met	Asn	Val	Cys	His
2585						2590					2595			
Ser	Leu	Ala	Ile	Asn	Ser	Ala	Leu	Pro	Gln	Asp	His	Arg	Asn	Asn
2600						2605					2610			
Leu	Asp	Glu	Ile	Ser	Asp	Ile	Phe	Ala	His	Gln	Lys	Val	Lys	Phe
2615						2620					2625			
Met	Phe	Gly	Phe	Ser	Glu	Asp	Lys	Gly	Arg	Ile	Leu	Gln	Ile	Phe
2630						2635					2640			
Ser	Ala	Ser	Ser	Phe	Ala	Ser	Lys	Phe	Asn	Ile	Leu	Asp	Phe	Phe
2645						2650					2655			
Ile	Asn	Asn	Ile	Leu	Leu	Leu	Met	Glu	Tyr	Ser	Ser	Thr	Tyr	Glu
2660						2665					2670			
Ala	Asn	Val	Trp	Lys	Thr	Arg	Tyr	Lys	Lys	Tyr	Val	Leu	Glu	Ser
2675						2680					2685			
Val	Phe	Thr	Ser	Asn	Ser	Phe	Leu	Ser	Ala	Arg	Ser	Ile	Met	Ile
2690						2695					2700			
Val	Gly	Ile	Met	Gly	Lys	Ser	Tyr	Ile	Thr	Glu	Gly	Leu	Cys	Lys
2705						2710					2715			

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Ala Met 2720	Leu Ile Glu Thr Met 2725	Lys Val Ile Ala Glu 2730	Pro Lys Ile
Thr Asp 2735	Glu His Leu Phe Leu 2740	Ala Ile Ser His Ile 2745	Phe Thr Tyr
Ser Lys 2750	Ile Val Glu Gly Leu 2755	Asp Pro Asn Leu Asp 2760	Leu Met Lys
His Leu 2765	Phe Trp Phe Ser Thr 2770	Leu Phe Leu Glu Ser 2775	Arg His Pro
Ile Ile 2780	Phe Glu Gly Ala Leu 2785	Leu Phe Val Ser Asn 2790	Cys Ile Arg
Arg Leu 2795	Tyr Met Ala Gln Phe 2800	Glu Asn Glu Ser Glu 2805	Thr Ser Leu
Ile Ser 2810	Thr Leu Leu Lys Gly 2815	Arg Lys Phe Ala His 2820	Thr Phe Leu
Ser Lys 2825	Ile Glu Asn Leu Ser 2830	Gly Ile Val Trp Asn 2835	Glu Asp Asn
Phe Thr 2840	His Ile Leu Ile Phe 2845	Ile Ile Asn Lys Gly 2850	Leu Ser Asn
Pro Phe 2855	Ile Lys Ser Thr Ala 2860	Phe Asp Phe Leu Lys 2865	Met Met Phe
Arg Asn 2870	Ser Tyr Phe Glu His 2875	Gln Ile Asn Gln Lys 2880	Ser Asp His
Tyr Leu 2885	Cys Tyr Met Phe Leu 2890	Leu Tyr Phe Val Leu 2895	Asn Cys Asn
Gln Phe 2900	Glu Glu Leu Leu Gly 2905	Asp Val Asp Phe Glu 2910	Gly Glu Met
Val Asn 2915	Ile Glu Asn Lys Asn 2920	Thr Ile Pro Lys Ile 2925	Leu Leu Glu
Trp Leu 2930	Ser Ser Asp Asn Glu 2935	Asn Ala Asn Ile Thr 2940	Leu Tyr Gln
Gly Ala 2945	Ile Leu Phe Lys Cys 2950	Ser Val Thr Asp Glu 2955	Pro Ser Arg
Phe Arg 2960	Phe Ala Leu Ile Ile 2965	Arg His Leu Leu Thr 2970	Lys Lys Pro
Ile Cys 2975	Ala Leu Arg Phe Tyr 2980	Ser Val Ile Arg Asn 2985	Glu Ile Arg
Lys Ile 2990	Ser Ala Phe Glu Gln 2995	Asn Ser Asp Cys Val 3000	Pro Leu Ala
Phe Asp 3005	Ile Leu Asn Leu Leu 3010	Val Thr His Ser Glu 3015	Ser Asn Ser
Leu Glu 3020	Lys Leu His Glu Glu 3025	Ser Ile Glu Arg Leu 3030	Thr Lys Arg
Gly Leu 3035	Ser Ile Val Thr Ser 3040	Ser Gly Ile Phe Ala 3045	Lys Asn Ser
Asp Met 3050	Met Ile Pro Leu Asp 3055	Val Lys Pro Glu Asp 3060	Ile Tyr Glu
Arg Lys 3065	Arg Ile Met Thr Met 3070	Ile Leu Ser Arg Met 3075	Ser Cys Ser

Ala

<210> SEQ ID NO 3

<211> LENGTH: 1278

<212> TYPE: DNA

<213> ORGANISM: *Saccharomyces cerevisiae*

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<220> FEATURE:
<221> NAME/KEY: misc_feature
<223> OTHER INFORMATION: GRE3 coding sequence

<400> SEQUENCE: 3

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aagcaaatag ttgtcagtgc aatccttcaa gacgattggg aaaatactgt aatataaatc      120
gtaaaggaaa attgaaaatt ttttaagat gtcttcactg gttactotta ataacggctc      180
gaaaatgccc ctagtccgct tagggtgctg gaaaattgac aaaaaagtct gtgcgaatca      240
aatztatgaa gctatcaaat taggctaccg tttattcgat ggtgcttgcg actacggcaa      300
cgaaaaggaa gttggtgaag gtatcaggaa agccatctcc gaaggcttg tttctagaaa      360
ggatatattt gttgtttcaa agttatggaa caattttcac catcctgac atgtaaaatt      420
agctttaaag aagaccttaa gcgatatggg acttgattat ttagacctgt attatatcca      480
cttcccaatc gccttcaaat atgttccatt tgaagagaaa taccctccag gattctatac      540
gggcgcagat gacgagaaga aaggtcacat caccgaagca catgtaccaa tcatagatac      600
gtaccgggct ctggaagaat gtgttgatga aggcttgatt aagtctattg gtgtttccaa      660
ctttcagga agcttgatc aagatttatt acgtggttgt agaatcaagc ccgtggcttt      720
gcaaattgaa caccatcctt atttgactca agaacaccta gttgagtttt gtaaattaca      780
cgatatecaa gtagtgtcct actcctcctt cggctcctcaa tcattcattg agatggactt      840
acagttggca aaaaccacgc caactctgtt cgagaatgat gtaatcaaga aggtctcaca      900
aaaccatcca ggcagtacca cttcccaagt attgcttaga tgggcaactc agagaggcat      960
tgccgtcatt ccaaaatcct ccaagaagga aaggttactt ggcaacctag aaatcgaaaa     1020
aaagttcact ttaacggagc aagaattgaa ggatatttct gactaaatg ccaacatcag     1080
atthaatgat ccatggacct ggttgatgg taaattcccc acttttgctt gatccagcca     1140
gtaaaatcca tactcaacga cgatatgaac aaattccct cattccgatg ctgtatatgt     1200
gtataaattt ttacatgctc ttctgtttag acacagaaca gctttaaata aaatggttga     1260
tatacttttt ctgcctgt                                     1278

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<210> SEQ ID NO 4
<211> LENGTH: 327
<212> TYPE: PRT
<213> ORGANISM: Saccharomyces cerevisiae

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<400> SEQUENCE: 4

Met Ser Ser Leu Val Thr Leu Asn Asn Gly Leu Lys Met Pro Leu Val
 1                5                10                15

Gly Leu Gly Cys Trp Lys Ile Asp Lys Lys Val Cys Ala Asn Gln Ile
 20                25                30

Tyr Glu Ala Ile Lys Leu Gly Tyr Arg Leu Phe Asp Gly Ala Cys Asp
 35                40                45

Tyr Gly Asn Glu Lys Glu Val Gly Glu Gly Ile Arg Lys Ala Ile Ser
 50                55                60

Glu Gly Leu Val Ser Arg Lys Asp Ile Phe Val Val Ser Lys Leu Trp
 65                70                75                80

Asn Asn Phe His His Pro Asp His Val Lys Leu Ala Leu Lys Lys Thr
 85                90                95

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Leu Ser Asp Met Gly Leu Asp Tyr Leu Asp Leu Tyr Tyr Ile His Phe
 100 105 110

Pro Ile Ala Phe Lys Tyr Val Pro Phe Glu Glu Lys Tyr Pro Pro Gly
 115 120 125

Phe Tyr Thr Gly Ala Asp Asp Glu Lys Lys Gly His Ile Thr Glu Ala
 130 135 140

His Val Pro Ile Ile Asp Thr Tyr Arg Ala Leu Glu Glu Cys Val Asp
 145 150 155 160

Glu Gly Leu Ile Lys Ser Ile Gly Val Ser Asn Phe Gln Gly Ser Leu
 165 170 175

Ile Gln Asp Leu Leu Arg Gly Cys Arg Ile Lys Pro Val Ala Leu Gln
 180 185 190

Ile Glu His His Pro Tyr Leu Thr Gln Glu His Leu Val Glu Phe Cys
 195 200 205

Lys Leu His Asp Ile Gln Val Val Ala Tyr Ser Ser Phe Gly Pro Gln
 210 215 220

Ser Phe Ile Glu Met Asp Leu Gln Leu Ala Lys Thr Thr Pro Thr Leu
 225 230 235 240

Phe Glu Asn Asp Val Ile Lys Lys Val Ser Gln Asn His Pro Gly Ser
 245 250 255

Thr Thr Ser Gln Val Leu Leu Arg Trp Ala Thr Gln Arg Gly Ile Ala
 260 265 270

Val Ile Pro Lys Ser Ser Lys Lys Glu Arg Leu Leu Gly Asn Leu Glu
 275 280 285

Ile Glu Lys Lys Phe Thr Leu Thr Glu Gln Glu Leu Lys Asp Ile Ser
 290 295 300

Ala Leu Asn Ala Asn Ile Arg Phe Asn Asp Pro Trp Thr Trp Leu Asp
 305 310 315 320

Gly Lys Phe Pro Thr Phe Ala
 325

<210> SEQ ID NO 5
 <211> LENGTH: 648
 <212> TYPE: DNA
 <213> ORGANISM: Saccharomyces cerevisiae
 <220> FEATURE:
 <221> NAME/KEY: misc_feature
 <223> OTHER INFORMATION: ISU1 coding sequence

<400> SEQUENCE: 5

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 catcagacct gtgaatgcca tgggggtttt gagagcgtcc agcataacga aaaggcttta 180
 tcatcccaag gtcatagagc attatacaca tccaagaaac gtcgggtcat tagataaaaa 240
 attgccaac gtcggcactg gtctagtggg tgcgccagcg tgcggtgatg tgatgaggtt 300
 gcagatcaaa gtcaacgact ctactggcgt tattgaagat gtcaaattca aaacttttgg 360
 atgtggctcc gccattgctt cctcttcata tatgactgaa ttggtacagg ggatgacctt 420
 ggacgatgcy gcaaaaatta agaacactga aattgctaag gagttgagct tgccccagct 480
 caagttgcat tgctctatgt tagcggaga tgccgatcaag gcagctatta aggactacaa 540
 atctaagaga aacactccaa ccatgttatc gtaatgaata agaagataac cgggacaaga 600
 acaagatcaa accctcacta atcaacaagt tggacttaat ttgtgcaa 648

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<210> SEQ ID NO 6
<211> LENGTH: 165
<212> TYPE: PRT
<213> ORGANISM: Saccharomyces cerevisiae

<400> SEQUENCE: 6

Met Leu Pro Val Ile Thr Arg Phe Ala Arg Pro Ala Leu Met Ala Ile
 1             5             10            15
Arg Pro Val Asn Ala Met Gly Val Leu Arg Ala Ser Ser Ile Thr Lys
          20            25            30
Arg Leu Tyr His Pro Lys Val Ile Glu His Tyr Thr His Pro Arg Asn
          35            40            45
Val Gly Ser Leu Asp Lys Lys Leu Pro Asn Val Gly Thr Gly Leu Val
          50            55            60
Gly Ala Pro Ala Cys Gly Asp Val Met Arg Leu Gln Ile Lys Val Asn
 65            70            75            80
Asp Ser Thr Gly Val Ile Glu Asp Val Lys Phe Lys Thr Phe Gly Cys
          85            90            95
Gly Ser Ala Ile Ala Ser Ser Ser Tyr Met Thr Glu Leu Val Gln Gly
          100           105           110
Met Thr Leu Asp Asp Ala Ala Lys Ile Lys Asn Thr Glu Ile Ala Lys
          115           120           125
Glu Leu Ser Leu Pro Pro Val Lys Leu His Cys Ser Met Leu Ala Glu
          130           135           140
Asp Ala Ile Lys Ala Ala Ile Lys Asp Tyr Lys Ser Lys Arg Asn Thr
          145           150           155           160
Pro Thr Met Leu Ser
          165

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<210> SEQ ID NO 7
<211> LENGTH: 729
<212> TYPE: DNA
<213> ORGANISM: Saccharomyces cerevisiae

<400> SEQUENCE: 7

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aattttcctt tgctaggtag aaccattaca acttcacat ctttccttac acataaactg    120
tcaaaggaag taaccagggc atcaacttcg cctccaagac caaagagaat tgttgcgca    180
attactggtg cgactggtgt tgcaactgga atcagacttc tacaagtgtt aaaagagttg    240
agcgtagaaa cccatttggg gatttcaaaa tgggggtgcag caacaatgaa atatgaaaca    300
gattgggaac cgcgatgaagt ggcggccttg gcaaccaaga catactctgt tcgtgatgtt    360
tctgcatgca tttcgtccgg atctttccag catgatggta tgattgttgt gccctgttcc    420
atgaaatcac tagctgctat tagaatcggg tttacagagg atttaattac aagagctgcc    480
gatgtttcga ttaaaagaaa tcgtaagtta ctactgggta ctcgggaaac ccccttatct    540
tccatccatc ttgaaaacat gttgtcttta tgcagggcag gtgttataat tttcctccg    600
gtacctgcgt tttatacaag acccaagagc cttcatgacc tattagaaca aagtgttggc    660
aggatcctag actgctttgg catccaagct gacacttttc ctcgttggga aggaataaaa    720
agcaagtaa                                     729

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<210> SEQ ID NO 8
<211> LENGTH: 242
<212> TYPE: PRT
<213> ORGANISM: Saccharomyces cerevisiae

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<400> SEQUENCE: 8

Met Leu Leu Phe Pro Arg Arg Thr Asn Ile Ala Phe Phe Lys Thr Thr
 1 5 10 15
 Gly Ile Phe Ala Asn Phe Pro Leu Leu Gly Arg Thr Ile Thr Thr Ser
 20 25 30
 Pro Ser Phe Leu Thr His Lys Leu Ser Lys Glu Val Thr Arg Ala Ser
 35 40 45
 Thr Ser Pro Pro Arg Pro Lys Arg Ile Val Val Ala Ile Thr Gly Ala
 50 55 60
 Thr Gly Val Ala Leu Gly Ile Arg Leu Leu Gln Val Leu Lys Glu Leu
 65 70 75 80
 Ser Val Glu Thr His Leu Val Ile Ser Lys Trp Gly Ala Ala Thr Met
 85 90 95
 Lys Tyr Glu Thr Asp Trp Glu Pro His Asp Val Ala Ala Leu Ala Thr
 100 105 110
 Lys Thr Tyr Ser Val Arg Asp Val Ser Ala Cys Ile Ser Ser Gly Ser
 115 120 125
 Phe Gln His Asp Gly Met Ile Val Val Pro Cys Ser Met Lys Ser Leu
 130 135 140
 Ala Ala Ile Arg Ile Gly Phe Thr Glu Asp Leu Ile Thr Arg Ala Ala
 145 150 155 160
 Asp Val Ser Ile Lys Glu Asn Arg Lys Leu Leu Leu Val Thr Arg Glu
 165 170 175
 Thr Pro Leu Ser Ser Ile His Leu Glu Asn Met Leu Ser Leu Cys Arg
 180 185 190
 Ala Gly Val Ile Ile Phe Pro Pro Val Pro Ala Phe Tyr Thr Arg Pro
 195 200 205
 Lys Ser Leu His Asp Leu Leu Glu Gln Ser Val Gly Arg Ile Leu Asp
 210 215 220
 Cys Phe Gly Ile His Ala Asp Thr Phe Pro Arg Trp Glu Gly Ile Lys
 225 230 235 240
 Ser Lys

<210> SEQ ID NO 9

<211> LENGTH: 1512

<212> TYPE: DNA

<213> ORGANISM: *Saccharomyces cerevisiae*

<400> SEQUENCE: 9

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 gatgacttaa tcgaaattac cgaagagatt gatccaaatc tcgaagtagg tgcaattatg 120
 aggaaggcct atgaatccca cttaccagcc cegttattta aaaatctcaa aggtgcttcg 180
 aaggatcttt tcagcatttt aggttgccca gccggttga gaagtaagga gaaaggagat 240
 catggtagaa ttgccatca tctggggctc gacccaaaaa caactatcaa ggaaatcata 300
 gattatttgc tggagtgtaa ggagaaggaa cctctcccc caatcactgt tcctgtgtca 360
 tctgcacctt gtaaacaca tatactttct gaagaaaaaa tacatctaca aagcctgcca 420
 acaccatata tacatgtttc agacggtggc aagtacttac aaacgtacgg aatgtggatt 480
 cttcaaaact cagataaaaa atggactaat tggteaattg cttagaggat ggtttagat 540
 gacaagcata tcaactgtct ggtaattaa ccacaacata ttagacaaat tgctgactct 600
 tgggcagcaa ttggaaaagc aaatgaatt ccttccgct tatgttttgg cgttccccca 660

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gcagctattt tagttagttc catgccaatt cctgaagggtg tttctgaatc ggattatggt 720
ggcgcaatct tgggtgagtc ggttccagta gtaaaatgtg agaccaacga tttaatgggt 780
cctgcaacga gtgagatggt atttgagggt actttgtcct taacagatac acatctggaa 840
ggcccatttg gtgagatgca tggatatggt ttcaaaagcc aaggtcatcc ttgtccattg 900
tacactgtca aggctatgag ttacagagac aatgctattc tacctgtttc gaaccccggt 960
ctttgtacgg atgagacaca taccttgatt ggttccactag tggtactga ggccaaggag 1020
ctggctattg aatctggctt gccaatctg gatgccttta tgccttatga ggctcaggct 1080
ctttggctta tcttaaagggt ggatttgaaa gggctgcaag cattgaagac aacgcctgaa 1140
gaatthtga agaaggtagg tgatatttac tttaggacaa aagttggttt tatagtccat 1200
gaaataattt tgggtggcaga tgatctgac atatttaact tcaaagaagt catctgggcc 1260
tacgttacia gacatacacc tgttgcatg cagatggctt ttgatgatgt cacttctttt 1320
cctttggctc cctttgtttc gcagtcaccc agaagtaaga ctatgaaagg tggaaagtgc 1380
gttactaatt gcatatttag acagcaatat gagcgcagtt ttgactacat aacttgtaat 1440
tttgaaaagg gatatccaaa aggattagtt gacaaagtaa atgaaaattg gaaaaggta 1500
ggatataaat aa 1512

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<210> SEQ ID NO 10

<211> LENGTH: 503

<212> TYPE: PRT

<213> ORGANISM: *Saccharomyces cerevisiae*

<400> SEQUENCE: 10

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Met Arg Lys Leu Asn Pro Ala Leu Glu Phe Arg Asp Phe Ile Gln Val
1          5          10          15
Leu Lys Asp Glu Asp Asp Leu Ile Glu Ile Thr Glu Glu Ile Asp Pro
20          25          30
Asn Leu Glu Val Gly Ala Ile Met Arg Lys Ala Tyr Glu Ser His Leu
35          40          45
Pro Ala Pro Leu Phe Lys Asn Leu Lys Gly Ala Ser Lys Asp Leu Phe
50          55          60
Ser Ile Leu Gly Cys Pro Ala Gly Leu Arg Ser Lys Glu Lys Gly Asp
65          70          75          80
His Gly Arg Ile Ala His His Leu Gly Leu Asp Pro Lys Thr Thr Ile
85          90          95
Lys Glu Ile Ile Asp Tyr Leu Leu Glu Cys Lys Glu Lys Glu Pro Leu
100         105         110
Pro Pro Ile Thr Val Pro Val Ser Ser Ala Pro Cys Lys Thr His Ile
115         120         125
Leu Ser Glu Glu Lys Ile His Leu Gln Ser Leu Pro Thr Pro Tyr Leu
130         135         140
His Val Ser Asp Gly Gly Lys Tyr Leu Gln Thr Tyr Gly Met Trp Ile
145         150         155         160
Leu Gln Thr Pro Asp Lys Lys Trp Thr Asn Trp Ser Ile Ala Arg Gly
165         170         175
Met Val Val Asp Asp Lys His Ile Thr Gly Leu Val Ile Lys Pro Gln
180         185         190
His Ile Arg Gln Ile Ala Asp Ser Trp Ala Ala Ile Gly Lys Ala Asn
195         200         205
Glu Ile Pro Phe Ala Leu Cys Phe Gly Val Pro Pro Ala Ala Ile Leu
210         215         220

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Val	Ser	Ser	Met	Pro	Ile	Pro	Glu	Gly	Val	Ser	Glu	Ser	Asp	Tyr	Val
225					230					235					240
Gly	Ala	Ile	Leu	Gly	Glu	Ser	Val	Pro	Val	Val	Lys	Cys	Glu	Thr	Asn
				245					250					255	
Asp	Leu	Met	Val	Pro	Ala	Thr	Ser	Glu	Met	Val	Phe	Glu	Gly	Thr	Leu
			260					265					270		
Ser	Leu	Thr	Asp	Thr	His	Leu	Glu	Gly	Pro	Phe	Gly	Glu	Met	His	Gly
		275					280					285			
Tyr	Val	Phe	Lys	Ser	Gln	Gly	His	Pro	Cys	Pro	Leu	Tyr	Thr	Val	Lys
	290					295					300				
Ala	Met	Ser	Tyr	Arg	Asp	Asn	Ala	Ile	Leu	Pro	Val	Ser	Asn	Pro	Gly
305					310					315					320
Leu	Cys	Thr	Asp	Glu	Thr	His	Thr	Leu	Ile	Gly	Ser	Leu	Val	Ala	Thr
				325					330					335	
Glu	Ala	Lys	Glu	Leu	Ala	Ile	Glu	Ser	Gly	Leu	Pro	Ile	Leu	Asp	Ala
			340					345					350		
Phe	Met	Pro	Tyr	Glu	Ala	Gln	Ala	Leu	Trp	Leu	Ile	Leu	Lys	Val	Asp
			355				360					365			
Leu	Lys	Gly	Leu	Gln	Ala	Leu	Lys	Thr	Thr	Pro	Glu	Glu	Phe	Cys	Lys
	370					375					380				
Lys	Val	Gly	Asp	Ile	Tyr	Phe	Arg	Thr	Lys	Val	Gly	Phe	Ile	Val	His
385					390					395					400
Glu	Ile	Ile	Leu	Val	Ala	Asp	Asp	Ile	Asp	Ile	Phe	Asn	Phe	Lys	Glu
				405					410					415	
Val	Ile	Trp	Ala	Tyr	Val	Thr	Arg	His	Thr	Pro	Val	Ala	Asp	Gln	Met
			420					425					430		
Ala	Phe	Asp	Asp	Val	Thr	Ser	Phe	Pro	Leu	Ala	Pro	Phe	Val	Ser	Gln
			435				440					445			
Ser	Ser	Arg	Ser	Lys	Thr	Met	Lys	Gly	Gly	Lys	Cys	Val	Thr	Asn	Cys
	450					455					460				
Ile	Phe	Arg	Gln	Gln	Tyr	Glu	Arg	Ser	Phe	Asp	Tyr	Ile	Thr	Cys	Asn
465					470					475					480
Phe	Glu	Lys	Gly	Tyr	Pro	Lys	Gly	Leu	Val	Asp	Lys	Val	Asn	Glu	Asn
				485					490					495	
Trp	Lys	Arg	Tyr	Gly	Tyr	Lys									
															500

We claim:

1. A recombinant yeast that has been genetically engineered to: ferment xylose and exhibit a reduced amount of functional PAD1 polypeptide, wherein the recombinant yeast has increased tolerance to gamma valerolactone (GVL) toxicity relative to a wild-type yeast or another recombinant yeast having the same genetic background but not exhibiting a reduced amount of functional PAD1 polypeptide.
2. The recombinant yeast of claim 1, further exhibiting a reduced amount of functional FDC1 polypeptide, wherein the recombinant yeast has increased tolerance to GVL toxicity relative to a wild-type yeast or another recombinant yeast having the same genetic background but not exhibiting reduced amounts of functional PAD1 and FDC1 polypeptides.
3. The recombinant yeast of claim 1, wherein the recombinant yeast comprises a disabling mutation in a gene encoding PAD1 polypeptide.
4. The recombinant yeast of claim 2, wherein the recombinant yeast further comprises a disabling mutation in a gene encoding FDC1 polypeptide.
5. The recombinant yeast of claim 3, wherein the PAD1 polypeptide is SEQ ID NO:8.
6. The recombinant yeast of claim 4, wherein the FDC1 polypeptide is SEQ ID NO:10.
7. The recombinant yeast of claim 1, further exhibiting reduced or undetectable amounts of functional ISU1, GRE3, and IRA2 polypeptides, wherein the recombinant yeast is capable of increased aerobic or anaerobic xylose fermentation relative to a wild-type yeast or another recombinant yeast not exhibiting reduced amounts of functional PAD1, ISU1, GRE3, and IRA2 polypeptides.
8. The recombinant yeast of claim 1, further comprising a disabling mutation at each of loci *isu1*, *gre3*, and *ira2*, whereby the mutations result in reduced amounts of functional ISU1, GRE3, and IRA2 polypeptides, respectively.
9. The recombinant yeast of claim 8, wherein the disabling mutation at the *gre3* locus comprises a substitution of

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a threonine for the alanine at amino acid residue position 46 of SEQ ID NO:4; wherein the disabling mutation at the *ira2* locus comprises a substitution of a stop codon for the glutamate at amino acid residue at position 2927 of SEQ ID NO:2; and wherein the disabling mutation at the *isu1* locus

comprises a substitution of a tyrosine for the histidine at amino acid residue position 138 of SEQ ID NO:6.

5 **10.** The recombinant yeast of claim **8**, wherein the recombinant yeast produces ethanol at an increased rate relative to a wild-type yeast or another recombinant yeast not exhibiting

reduced or undetectable amounts of functional ISU1, GRE3, and IRA2 polypeptides.

10 **11.** The recombinant yeast of claim **10**, wherein the increased rate of ethanol production occurs under anaerobic conditions.

15 **12.** The recombinant yeast of claim **1**, wherein the recombinant yeast is of the genus *Saccharomyces*.

13. The recombinant yeast of claim **12**, wherein the recombinant yeast is of the species *Saccharomyces cerevisiae*.

20 **14.** The recombinant yeast of claim **3**, wherein a portion of an extrachromosomal vector stably maintained in the recombinant yeast comprises the disabling mutation.

15. The recombinant yeast of claim **3**, wherein a nucleic acid sequence comprising the disabling mutation is integrated into a chromosome of the recombinant yeast.

60

16. A yeast inoculum, comprising: (a) a recombinant yeast of claim **1**; and (b) a culture medium.

17. A method for fermenting cellulosic material into ethanol, comprising contacting a GVL-treated hydrosylate to the recombinant yeast of claim **1** or the yeast inoculum of claim **16** for a period of time sufficient to allow fermentation of at least a portion of the cellulosic material to ethanol, whereby the rate of fermentation of cellulosic material of the GVL-treated hydrosylate to ethanol is increased relative to the fermentation rate of a GVL-treated hydrosylate not contacted to the recombinant yeast or the yeast inoculum.

18. The method of claim **17**, further comprising separating the ethanol from fermented cellulosic material.

15 **19.** The method of claim **17**, wherein the GVL-treated hydrosylate comprises xylose.

20. The method of claim **17**, wherein the recombinant yeast is *Saccharomyces cerevisiae*.

21. The method of claim **17**, wherein the cellulosic material comprises lignocellulosic biomass.

20 **22.** The method of claim **21**, wherein the lignocellulosic biomass comprises at least one material selected from the group consisting of agricultural residues, wood, municipal solid wastes, paper and pulp industry wastes, and herbaceous crops.

* * * * *